

DAFTAR PUSTAKA

- Aji, B.K., dan Kurniawan, F., 2012, Pemanfaatan Serbuk Biji Salak (*Salacca Zalacca*) sebagai adsorben Cr(VI) dengan Metode Batch dan Kolom, *Jurnal Sains Pomits*, **1**(1).
- Andreas, A., Ryan, dan Koleangan A.A., 2005, *Sintesis dan Modifikasi Karbon Aktif dari Limbah Kulit Pisang untuk Aplikasi sebagai Adsorben Zat Warna*, Chemical Engineering Department, Parahyangan Catholic University, Bandung.
- Annadurai, G., Juang, R., dan Lee, D., 2002, Use of Cellulose-Based Wastes For Adsorption of Dyes From Aqueous Solution, *J. Hazardous Materials*, 263-274.
- Arini, D.I.D., 2012, Potensi Pangi (*Pangium edule Reinw*) sebagai Bahan Pengawet Alami dan Prospek Pengembangannya di Sulawesi Utara, *Info BPK Manado*, **2**(2): 103-114.
- Asbahani, 2013, Pemanfaatan Limbah Ampas Tebu sebagai Karbon Aktif untuk Menurunkan Kadar Besi pada Air Sumur, *Jurnal Teknik Sipil*, **13**(1).
- Asip, F., Mardhiah, R., dan Husna, 2008, Uji Efektivitas Cangkang Telur dalam Mengadsorpsi Ion Fe dengan Proses Batch, *Jurnal Teknik Kimia*, **15**(2): 22-26.
- Astuti, W., 2016, *Pemanfaatan Karbon Aktif dari Tempurung Kluwak (Pangium edule Reinw) sebagai Adsorben Zat Warna Rhodamin B*, Skripsi tidak diterbitkan, Fakultas Matematika dan Ilmu Pengetahuan Alam, Universitas Hasanuddin, Makassar.
- Atkins, P.W., 1999, *Kimia Fisika Jilid 2*, Erlangga, Jakarta
- Cahyadi, W., 2006, *Analisis dan Aspek Kesehatan Bahan Tambahan Pangan*, PT Bumi Aksara, Jakarta.
- Departemen Perindustrian dan Perdagangan, 2003, *Syarat Mutu dan Uji Arang Aktif SII NO. 0258-88*, Balai Perindustrian dan Perdagangan, Palembang.
- Edwin, E., Sherliy., Liong, S., dan Taba, P., 2005, Pemanfaatan Karbon Aktif Tempurung Kenari Sebagai Adsorben Fenol dan Klorofenol dalam Perairan, *Marina Chimica Acta*, **6**(1): 9-15.



B., 2008, *Analisis Rhodamin B dalam Saos dan Cabe Giling di Pasar Kecamatan Laweyan Kotamadya Surakarta dengan Metode Kromatografi Lapis Tipis*, Skripsi, Fakultas Farmasi UMS, Solo.

Gupta, S.S., dan Bhattacharyya, K.G., 2008, Immobilization of Pb (II), Cd (II) and Ni (II) Ions on Kaolinite and Montmorillonite Surfaces from Aqueous Medium, *Journal of Environmental Management* 87, 46-58.

Habibah, M.D., Nurdiana, H., Rohmawati, L., dan Setyarsih, W., 2014, Sintesis Nanopori Karbon Aktif dari Tempurung Kluwak (*Pangium edule*), Prosiding Seminar Nasional Fisika dan Pendidikan Fisika (SNFPPF), 5(1): 30-32.

Hadiwidodo, M., 2008, Penggunaan Abu Sekam Padi Sebagai Adsorben dalam Pengolahan Air Limbah yang Mengandung Logam Cu, *Jurnal Teknik*, 29: 55-63.

Hajar, E.W.I., Sitorus, R.S., Mulianingias, N., dan Welan, F. J., 2016, Efektivitas Adsorpsi Logam Pb^{2+} dan Cd^{2+} Menggunakan Media Adsorben Cangkang Telur Ayam, *Konversi*, 5(1): 1-7.

Hala, Y., Taba, P., dan Susilowati, B.A., 2010, Adsorpsi Rhodamin B dalam Air oleh Karbon Aktif Tempurung Kemiri, *Jurnal Alam dan Lingkungan*, 1(2): 41-50.

Harti, R., Allwar, dan Fitri, N., 2014, Karakterisasi Dan Modifikasi Karbon Aktif Tempurung Kelapa Sawit Dengan Asam Nitrat Untuk Menjerap Logam Besi Dan Tembaga Dalam Minyak Nilam, *Chemical Research – Inco.J.Chem.Res*, 1(2): 74-83.

Hasanudin dan Rachmat A., 2010, Isoterm Adsorpsi Desorpsi dan Porositas Katalis Ag-TiO₂/Zeolit, *Isotermal Adsorpsi-Desorpsi* 7(2): 17-25.

Hastomo, A.E., 2008, *Analisis Rhodamin B dan Metanil Yellow dalam Jelly di Pasar Kecamatan Jebres Kota Madya Surakarta dengan Metode Kromatografi Lapis Tipis*, Skripsi tidak diterbitkan, Universitas Muhammadiyah Surakarta, Surakarta.

Ina, A.T., Yulianti, L.I.M., dan Pranata, F.S., 2013, *Pemanfaatan Pektin Kulit Buah Jeruk Siam (Citrus nobilis var. Microcarpa) sebagai Adsorben Logam Tembaga (Cu)*, Skripsi, Fakultas Teknologi Universitas Atma Jaya, Yogyakarta.

Ismanto, A.E., Wang, S., Soetaredjo, F.E., Ismadji, S., 2010, Preparation of Capacitor's Electrode from Cassava Peel Waste, *Bioresour. Technol.*, 101: 3534-3540.

R.H., 2016, *Pembuatan dan Karakterisasi Karbon Aktif dari Tempurung Kelapa (Cocous nacificera L.) Sebagai Adsorben Zat Warna Metilen Biru*, Skripsi tidak diterbitkan, Universitas Lampung, Bandar Lampung.



- Kurniati, E., 2008, Pemanfaatan Cangkang Kelapa Sawit Sebagai Arang Aktif, *Jurnal Penelitian Ilmu Teknik*, **8**(2): 96-103.
- Labanni, A., Zakir, M. dan Maming, 2015, Sintesis dan Karakterisasi Karbon Nanopori Ampas Tebu (*Saccharum officinarum*) dengan Aktivator $ZnCl_2$ melalui Iradiasi Ultrasonik sebagai Bahan Penyimpan Energi Elektrokimia, *Indo. Chim.Acta*, **8**(1): 1-9.
- Lacerda, V.S., Sotelo, JB.L., Guimaraes, A.C., Navarro, S.H., Bascones, M.S., Gracia, LM.N., Ramos, P.M., and Gil, J.M., 2015, Rhodamine B Removal with Activated Carbons Obtained from Lignocellulosic Waste, *J. of Environmental Management*, 67-76.
- Latifan, R., dan Susanti, D., 2012, Aplikasi Karbon Aktif dari Tempurung Kluwak (*Pagium Edule*) dengan Variasi Temperatur Karbonisasi dan Aktivasi Fisika sebagai Electric Double Layer Capacitor (EDLC), *Jurnal Teknik Material dan Metalurgi*, **1**(1): 1-6.
- Liem, V., Putranto, A., and Andreas, A., 2015, *Sintesis Karbon Aktif dari Kulit Salak Aktivasi Kimia Senyawa KOH sebagai Adsorben Proses Adsorpsi Zat Warna Metilen Biru*, Seminar Nasional Teknik Kimia, Universitas Katolik Parahyangan, Bandung.
- Liu, Y., Hu, Z., Xu, K., Zheng, X., Gao, Q., 2008, Surface Modification and Performance of Activated Carbon Electrode Material, *Acta Phys. Chim. Sinica*, **24**(7): 1143-1148.
- Maulana, A., 2011, *Pembuatan Karbon Aktif Berbahan Dasar Petroleum Coke dengan Metoda Aktivasi Kimia*, Skripsi, Teknik Kimia UI, Depok.
- Maulinda, L., ZA, N., dan Sari, D. N., 2015, Pemanfaatan Kulit Singkong Sebagai Bahan Baku Karbon Aktif, *Jurnal Teknologi Kimia Unimal*, **4**(2): 11-19.
- Mohammadi, M., Hassani, A.J., Abdul, R.M., and Ghasem, D.N., 2010, Removal of Rhodamine B from Aqueous Solution Using Palm Shell-Based Activated Carbon; Adsorption and Kinetic Studies, *J.Chem. Eng*, **55**(12), 5777-5786.
- Monk, P., 2004, *Physical Chemistry*, John Wiley dan Sons, Inc, New York.
- Mufrodi, Z., Widiastuti, N., dan Kardika, R.C., 2008, *Adsorpsi Zat Warna Tekstil dengan Menggunakan Abu Terbang (Fly Ash) Untuk Variasi Massa Adsorben dan Suhu Operasi*, Skripsi tidak diterbitkan, Program Studi Teknik Kimia Fakultas Teknologi Industri, Universitas Ahmad Dahlan, Yogyakarta.



- Muna, A.N., 2011, *Kinetika Adsorpsi Karbon Aktif dari Batang Pisang sebagai Adsorben untuk Penyerapan Ion Logam Cr (VI) pada Air Limbah Industri*, Tugas Akhir II, Fakultas MIPA, Universitas Semarang, Semarang.
- Namasivayam, C., 2001, Uptake of Dyes by a Promosing Locally Available Agriculture Solid Waste: Coir Pith, *Waste Manage*, **21**(4): 381-387.
- Nurdiansah, H., dan Susanti, D., 2003, Pengaruh Variasi Temperatur Karbonisasi dan Temperatur Aktivasi Fisika dari Elektroda Karbon Aktif Tempurung Kelapa dan Tempurung Kluwak Terhadap Nilai, *Jurnal Teknik Pomits*, **2**(1): 13-18.
- Nurmasari, R., Astuti, M.D., Umaningrum, D., dan Khusnaria, D.A., 2014, Kajian Adsorpsi Rhodamin B pada Humin, *Prosiding Seminar Nasional Kimia*, 203-210.
- Prasetyo, A., Yudi, A., dan Astuti, R.N., 2011, Adsorpsi Metilen Blue pada Karbon Aktif dari Ban Bekas dengan Variasi Konsentrasi NaCl pada Suhu Pengaktifan 600 °C dan 650 °C, *Jurnal Neutrino*, **4**(1): 16-23.
- Pratiwi, Y., 2010, Penentuan Tingkat Pencemaran Limbah Industri Tekstil berdasarkan Nutriion Value Coefisient Bioindikator, *Jurnal Teknologi*, **3**(2): 129-137.
- Purnawati, 2011, *Optimalisasi Adsorpsi Zat Warna Rhodamin B oleh Biomassa Chlorella sp yang diimbolisasi dalam Silika Gel*, Skripsi tidak diterbitkan, Universitas Negeri Semarang.
- Purnamawati, H., dan Utami, B., 2014, Pemanfaatan Limbah Kulit Buah Kakao (*Theobroma cocoa L.*) sebagai Adsorben Zat Warna Rhodamin B, *Prosiding Seminar Nasional Fisika dan Pendidikan Fisika (SNFPF)*, **5**(1):12-18, FKIP Universitas Sebelas Maret, Surakarta.
- Putranto, A. dan Angelina, S., 2014, Pemodelan Perpindahan Massa Adsorpsi zat warna pada Florisil dan Silica Gel dengan Homogeneous and Heterogeneous Surface Diffusion Model, *Lembaga Pendidikan dan Pengabdian kepada Masyarakat*, **2**(3).
- Qu, D., Shi, H., 1998, *Studies of Activated Carbons Used in Double Layer Capacitors*, *J. Power Sources*, **74**: 99-107.
- Purnawati, E., 2007, *Pemanfaatan Kitosan Hasil Deasitulasi Kitin Cangkang Bekicot Sebagai Adsorben Zat Warna Remozol Yellow*, Skripsi tidak diterbitkan, Universitas Sebelas Maret.



- Ramdja, A.F., Halim, M., dan Handi, J., 2008, Pembuatan Karbon Aktif dari Pelepah Kelapa (*Cocos nucifera*), *Jurnal Teknik Kimia*, **15**(2): 1-8.
- Saefudin, Trisna, dan Kusnadi. 2000. Pengaruh pH dan Waktu Kontak terhadap Biosorpsi Logam Zn oleh Biomassa *Aspergillus niger* Van Tregthem pada Larutan Limbah Pertambangan Nikel. BandungUPI.
- Setiawati, E., dan Suroto, 2010, Pengaruh Bahan Aktivator pada Pembuatan Karbon Aktif Tempurung Kelapa, *Jurnal Riset Industri Hasil Hutan*, **2**(1): 21-26.
- Setyadhi, L., Wibowo, D., dan Ismadji, S., 2005, Modifikasi Sifat Kimia Permukaan Karbon Aktif dengan Asam Oksidator dan Non-oksidator serta Aplikasinya Terhadap Adsorpsi Methylene Blue, *Design and Application of Technology*.
- Shofa, 2012, *Pembuatan Karbon Aktif Berbahan Baku Ampas Tebu dengan Aktivasi Kalium Hidroksida*, Skripsi, Program Studi Teknik Kimia Fakultas Teknik, Universitas Indonesia, Depok.
- Singh, K.P., Malik, A., Sinha, S., dan Ojha, P., 2008, Liquid-phase Adsorption of Phenols Using Activated Carbons Derived from Agricultural Waste Material, *J. Hazard Mater*, **150**(3): 626-641.
- Sinta, I.N., Suarya, P., dan Santi, S.S., 2015, Adsorpsi Ion Fosfat oleh Lempung Teraktivasi Asam Sulfat (H_2SO_4), *Jurnal Kimia*, **9**(2): 217-225.
- Sudrajat, R., dan Pari, G., 2011, *Arang aktif Teknologi pengolahan dan masa depannya*, Badan Penelitian dan Pengembangan Kehutanan, Jakarta.
- Sulistyawati, S., 2008, *Modifikasi Tongkol Jagung sebagai Adsorben Logam Berat Pb(II)*, Skripsi, Departemen Kimia, Institut Pertanian Bogor.
- Surest, A. H., Permana, I., dan Wibisono, R. G., 2010, Pembuatan Karbon Aktif Dari Cangkang Biji Ketapang, *Jurnal Teknik Kimia*, **17**(4): 1-11.
- Tanasal, A.M., Nafie, N.L., dan Taba, P., 2015 Biosorpsi Ion Logam Cd(II) oleh Kulit Buah Naga. Skripsi, Jurusan Kimia, Universitas Hasanuddin, Makassar.
- Tanasale, M., Sutapa, I.W., dan Topurtawy, R.R., 2014, Adsorpsi Zat Warna Rhodamin B oleh Karbon Aktif dari Kulit Durian (*Durio zibethinus*), *Ind. J. Chem. Res.*, **2**(1): 116-121.

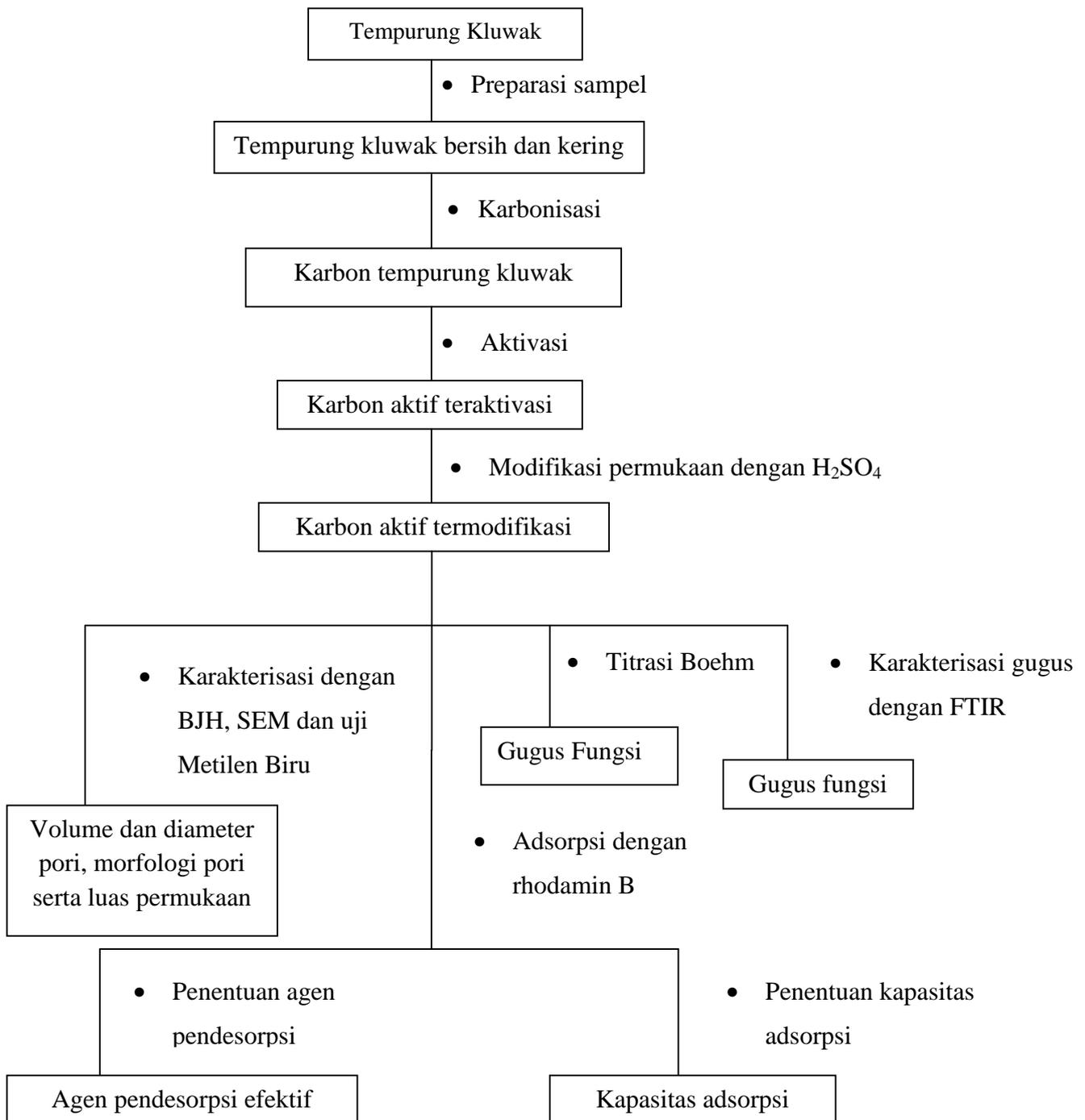
A., dan Kaur, H., 2017, Response Surface Optimization of Rhodamine B Dye Removal Using Paper Industry Waste as Adsorbent, *Int J Ind Chem*.



- Wibowo, N., Setiawan, J. dan Ismadji, S. 2004, Modifikasi Gugus Aktif Suatu Karbon Aktif dan Karakterisasinya. *J. Tek. Kim. Ind.*, **3**(1): 39-46.
- Widjanarko, Widianoro, dan Soetaredjo, 2006, Kinetika Adsorben Zat Warna Congo Red dan Rhodamin B dengan Menggunakan Serabut Kelapa dan Tebu, *Jurnal Teknik Kimia*, Skripsi tidak diterbitkan, Universitas Katolik Widya Mandala, Surabaya.
- Wulandari, R., 2016, Penentuan Kapasitas Spesifik Karbon Aktif Tempurung Kemiri (*Alleurites mollucana*) hasil modifikasi dengan HNO₃, H₂SO₄ dan H₂O₂ menggunakan metode Cyclic Voltammetry, *Skripsi tidak diterbitkan*, Jurusan Kimia, Fakultas Matematika dan Ilmu Pengetahuan Alam Universitas Hasanuddin.
- Zakaria, Ahmad., 2011, *Adsorpsi Cu (II) Menggunakan Zeolit Sintetis dari Abu Terbang Batu Bara*, Tesis Sekolah Pascasarjana, Institut Pertanian Bogor, Bogor.

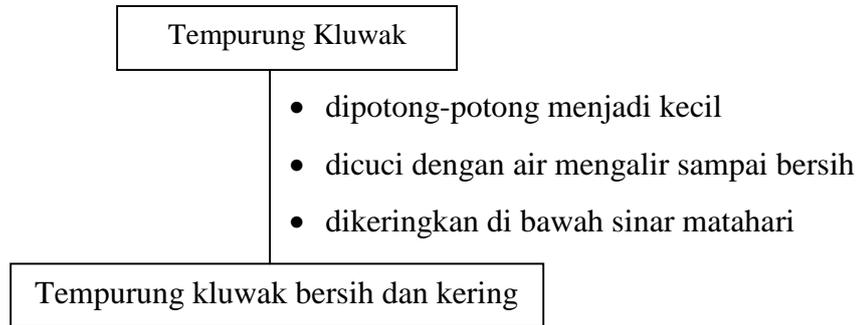


Lampiran 1. Diagram Alir Penelitian

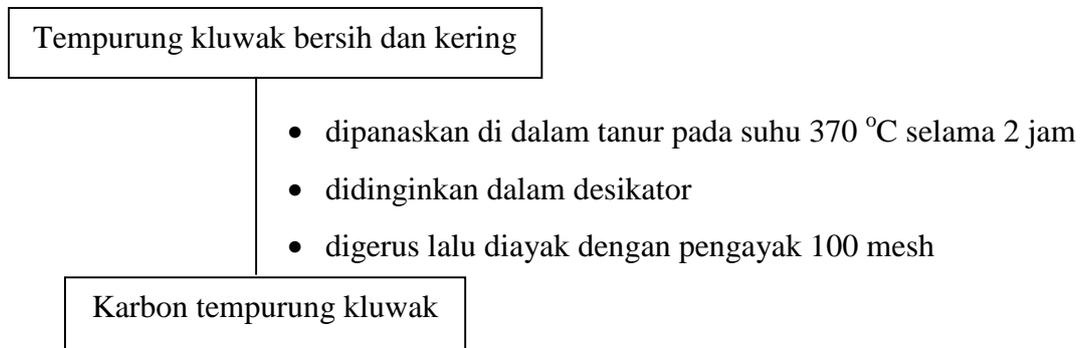


Lampiran 2. Skema Kerja Penelitian

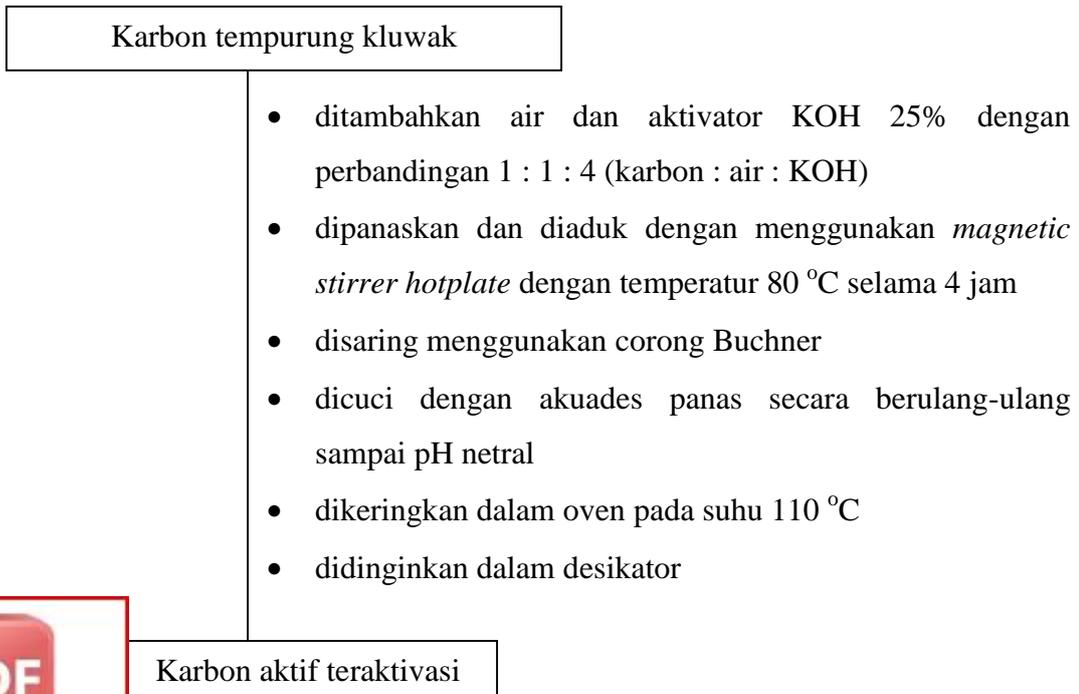
a. Preparasi Sampel



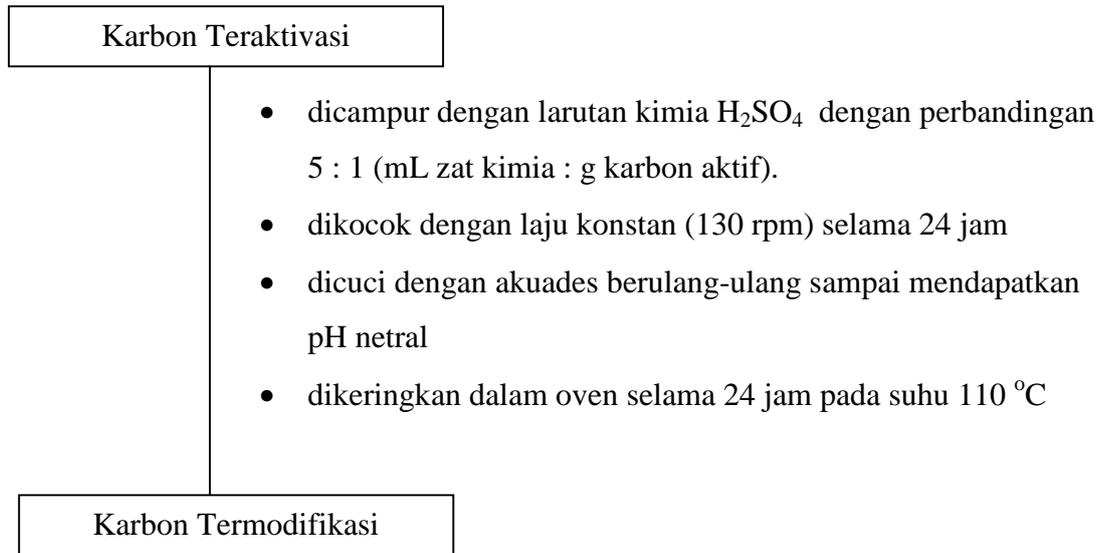
b. Karbonisasi



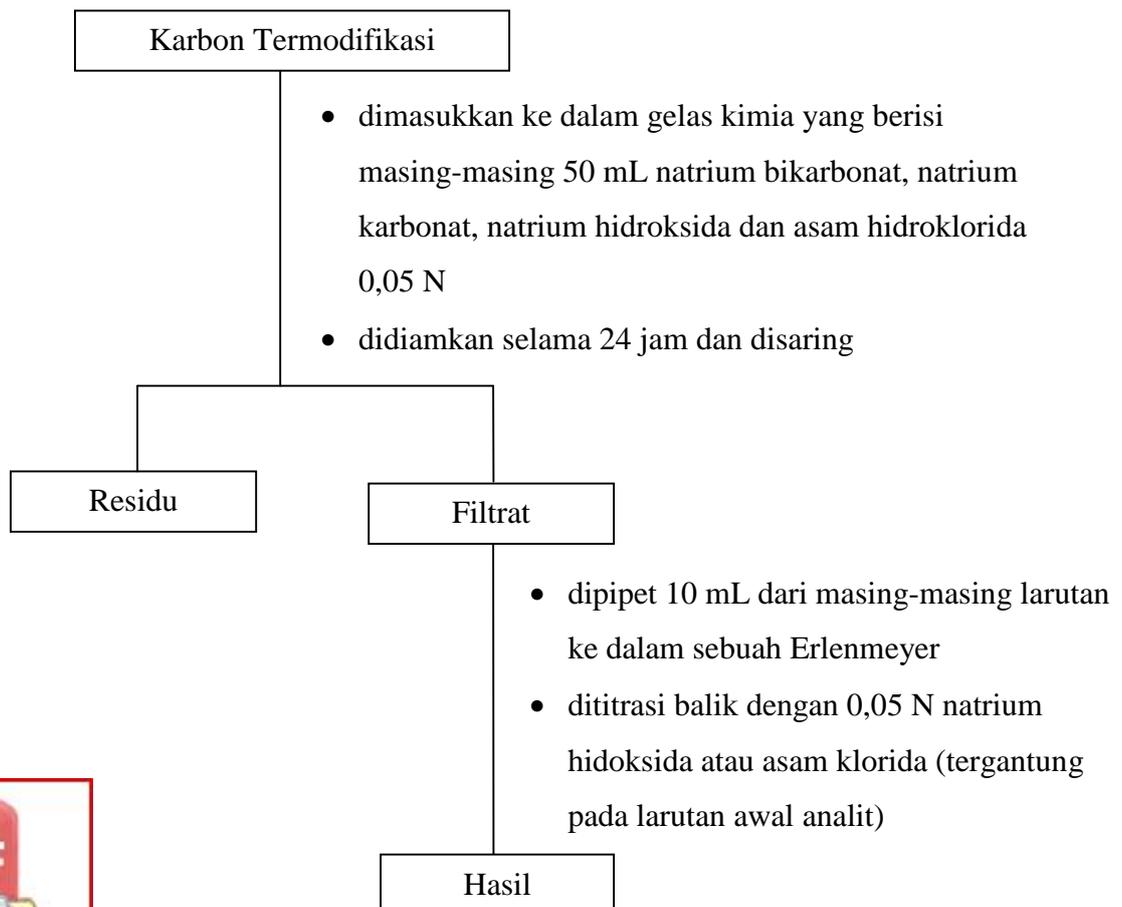
c. Aktivasi



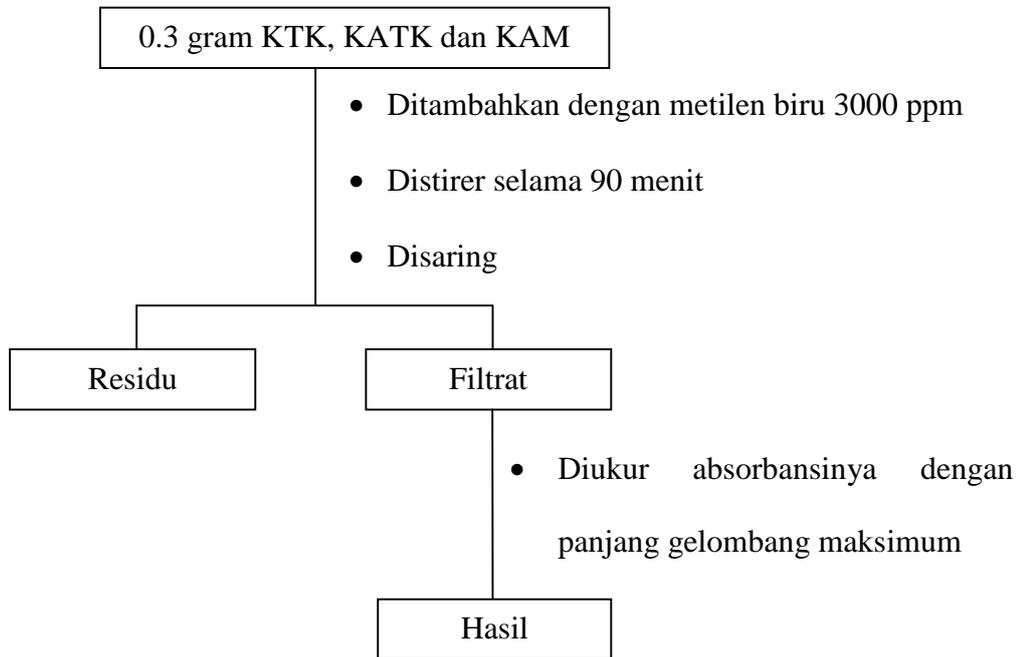
d. Modifikasi Permukaan



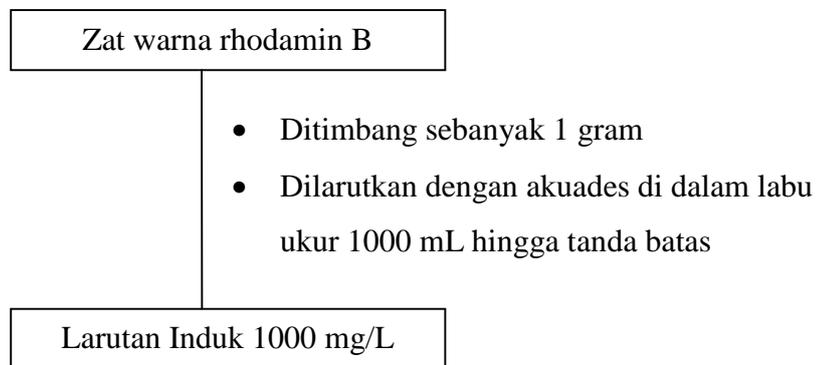
e. Skema Kerja Titrasi Boehm



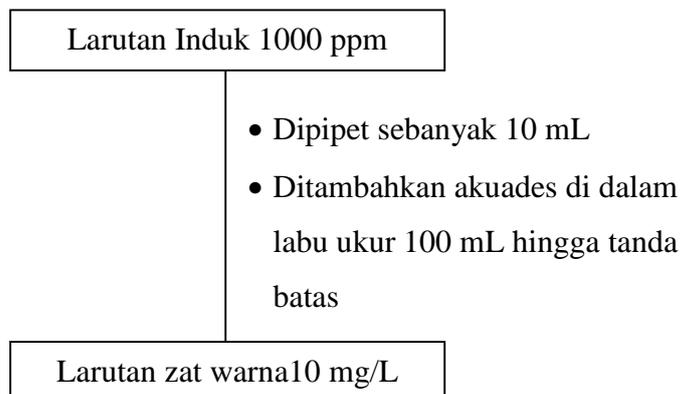
f. Skema Kerja Luas Permukaan dengan Metilen Biru



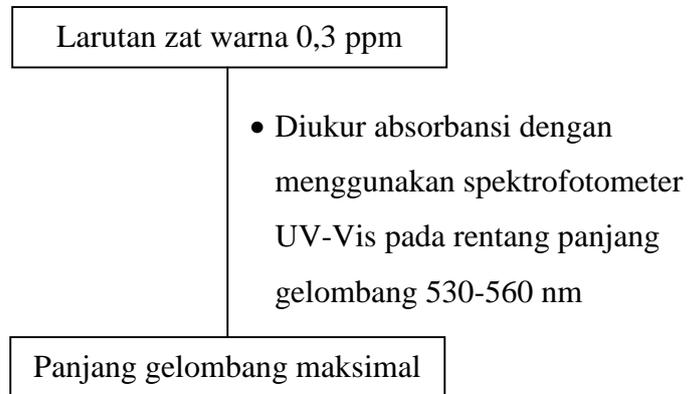
g. Pembuatan Larutan Induk 1000 ppm



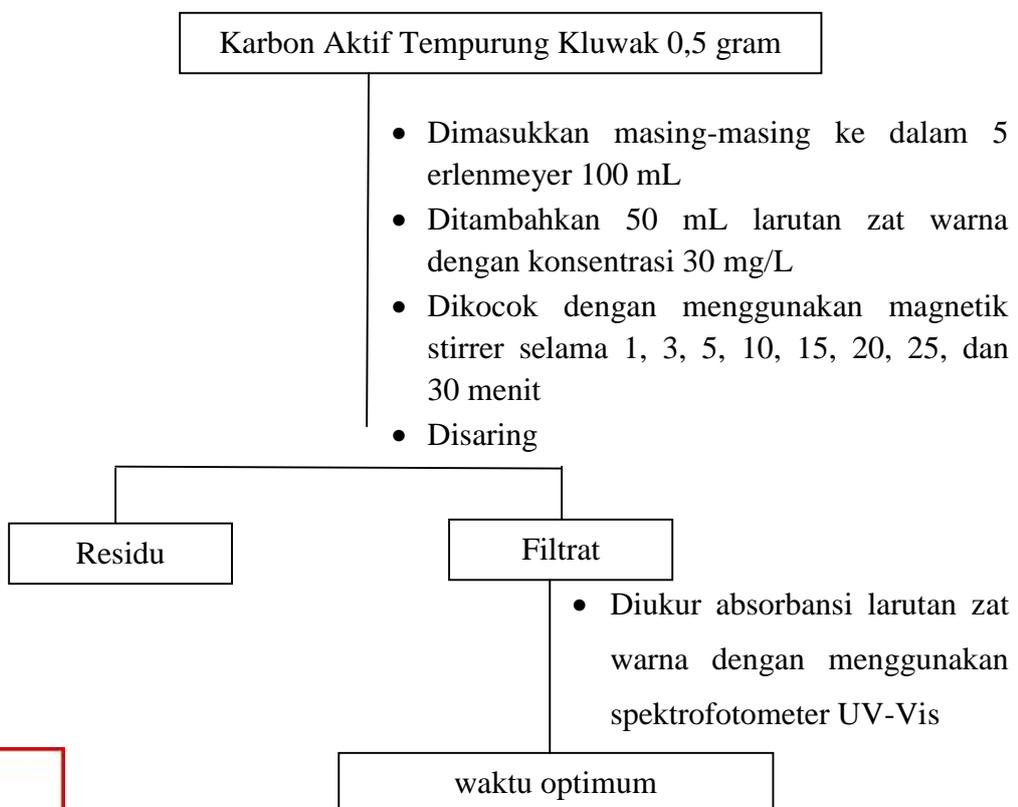
h. Pembuatan Larutan Zat Warna 10 ppm



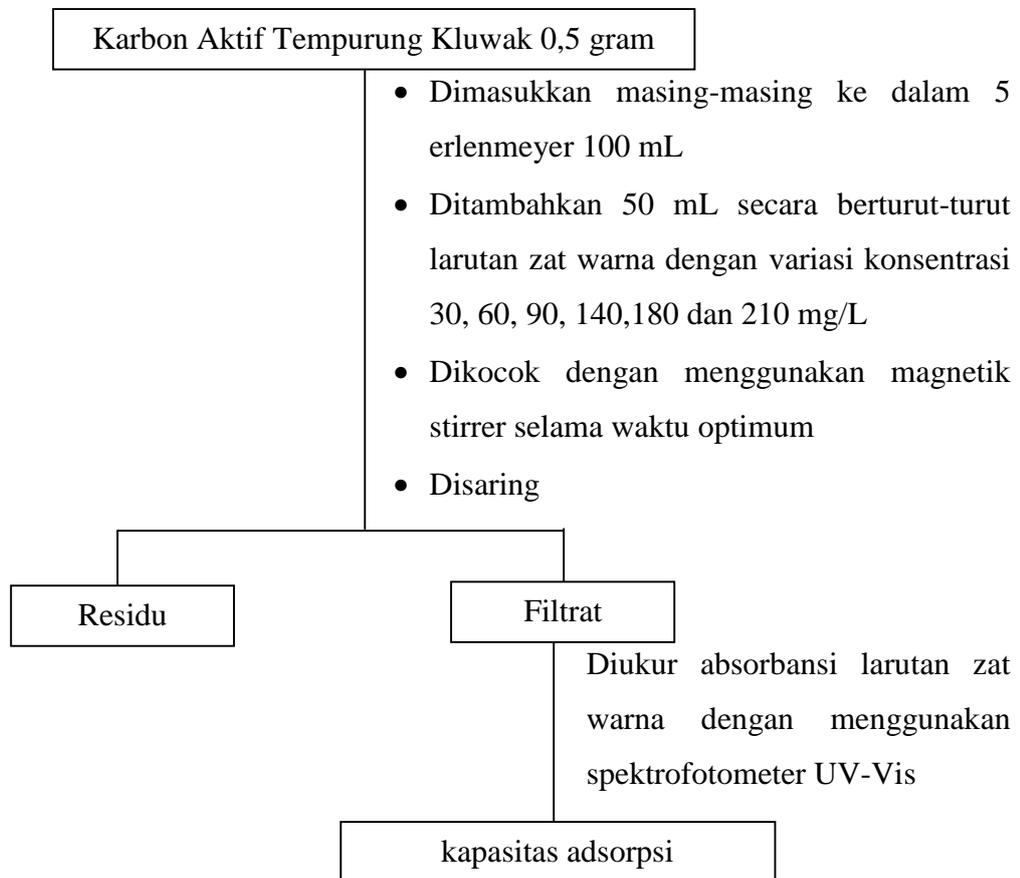
i. Penentuan Panjang Gelombang Maksimum



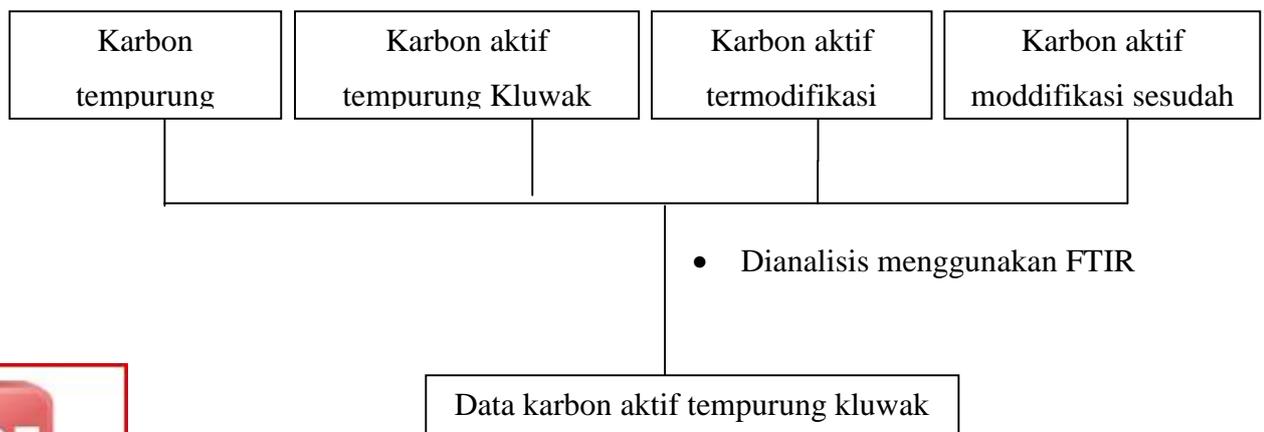
j. Penentuan Waktu Kontak Optimum



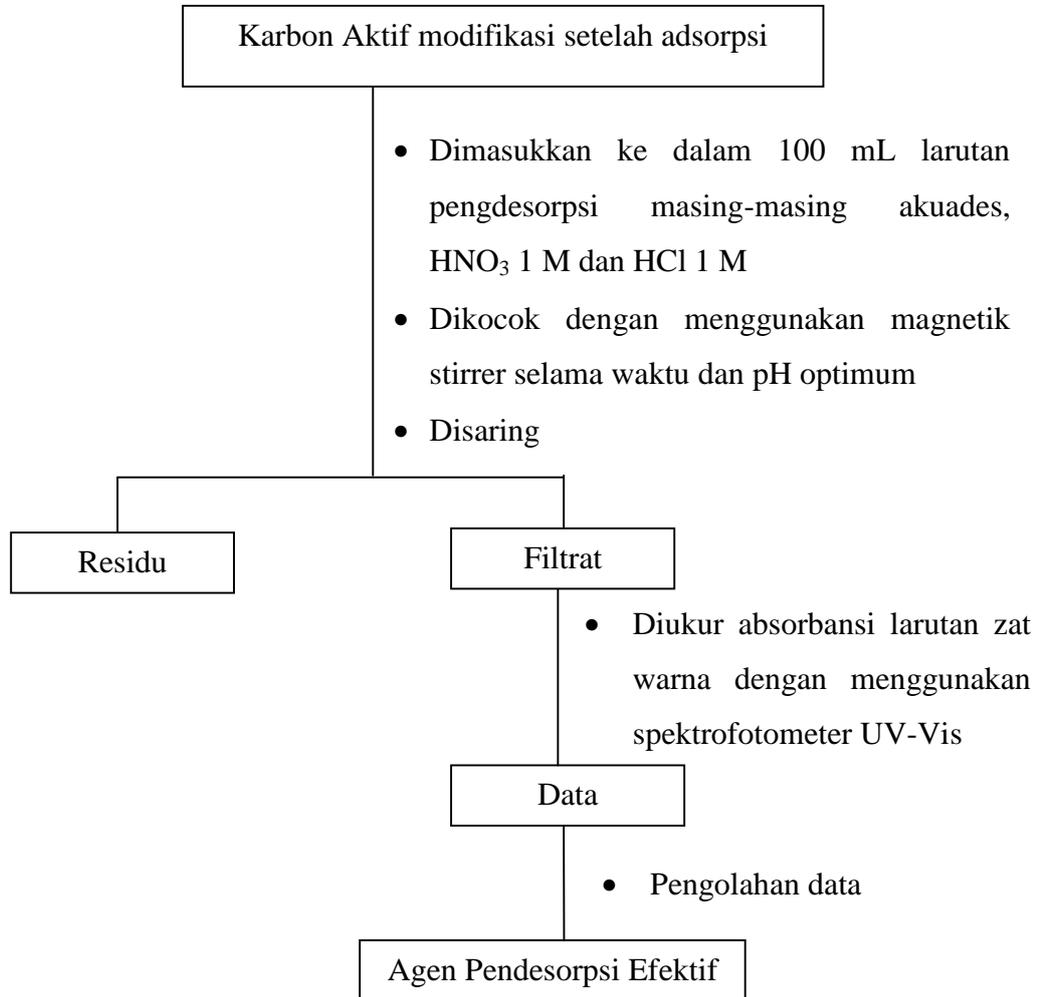
k. Penentuan Kapasitas Adsorpsi



l. Karakterisasi Gugus dengan FTIR



m. Desorpsi



Lampiran 3. Dokumentasi Penelitian



Limbah tempurung kluwak



Karbon tempurung kluwak



Karbon hasil ayakan



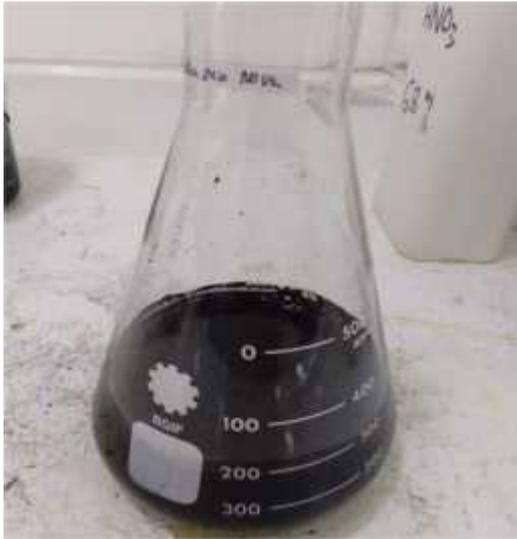
Proses aktivasi



Proses penyiangan karbon aktif



Karbon aktif



Proses modifikasi



Proses penyaringan karbon modifikasi



Karbon modifikasi



Titration Boehm total acid



Titration Boehm total base



Uji metilen biru





Larutan rhodamin B 30 ppm



Proses optimasi waktu



Hasil optimasi waktu



Larutan rhodamin B untuk proses kapasitas adsorpsi



Pengadukan dengan multistirer



Hasil larutan setelah pengadukan





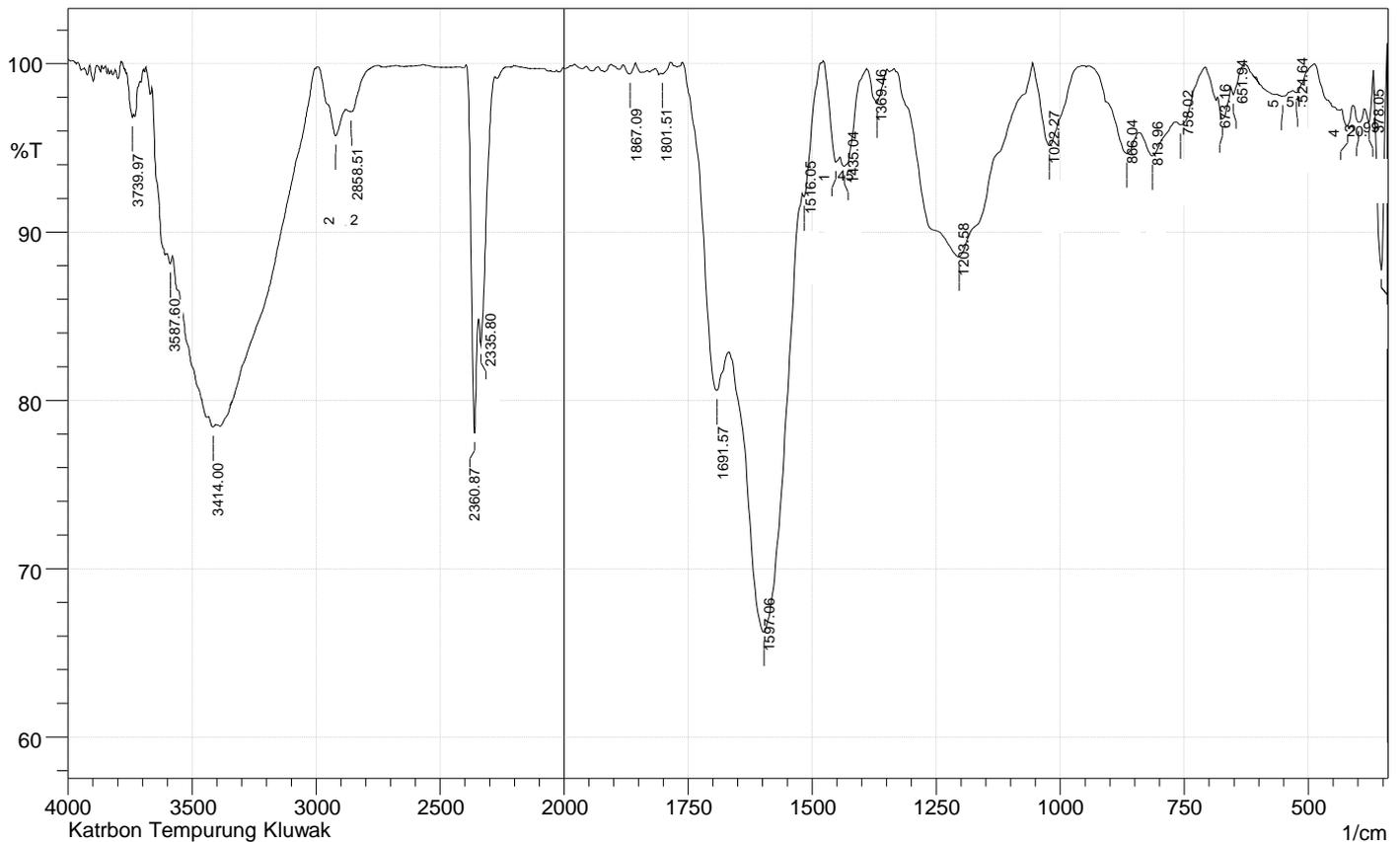
Proses desorpsi



Hasil desorpsi



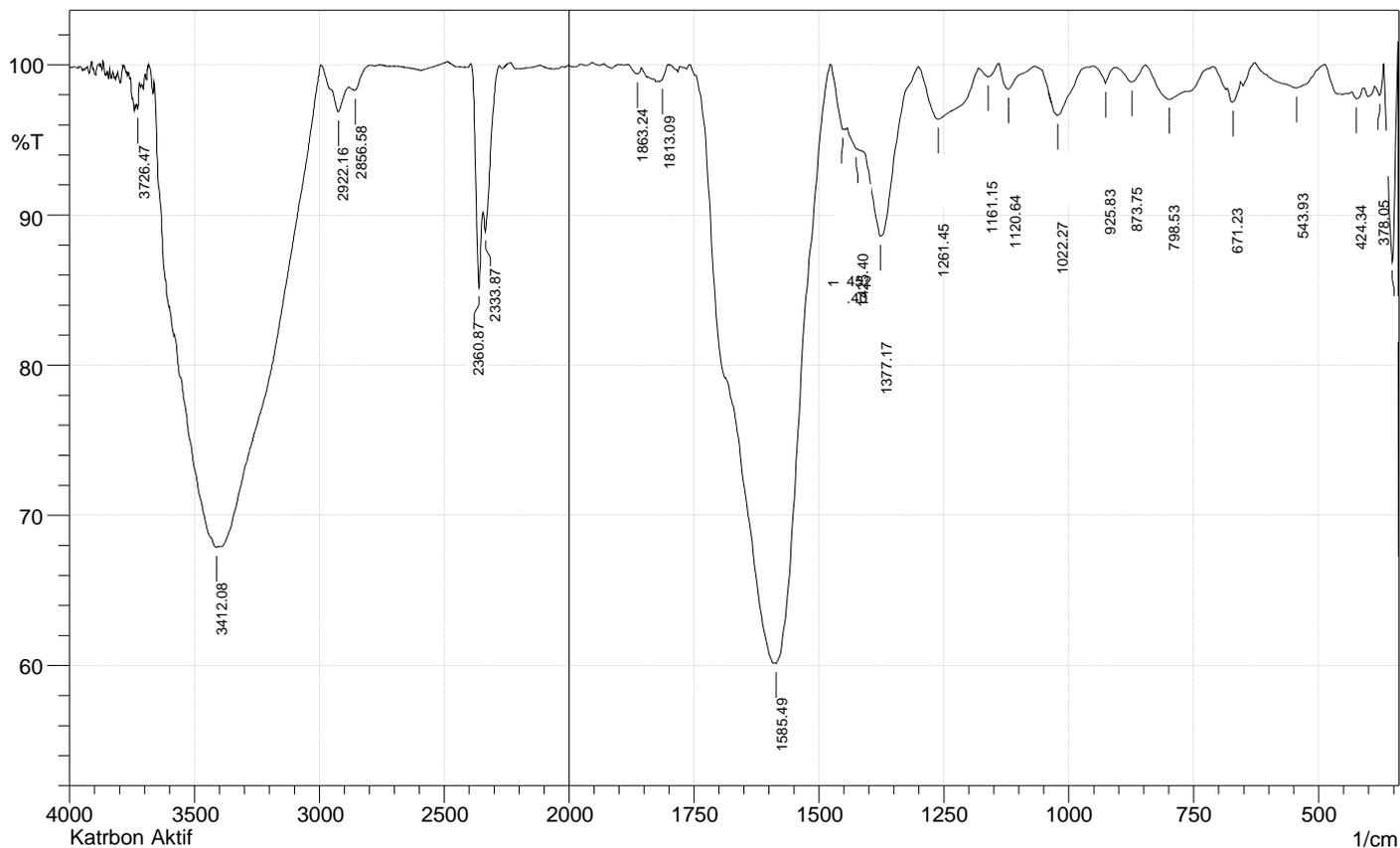
Lampiran 4. Spektrum FTIR dari KTK



No.	Peak	Intensity	Corr. Intensity	Base (H)	Base (L)	Area	Corr. Area
1	352.97	87.706	11.681	368.4	343.33	0.86	0.796
2	378.05	96.497	1.819	385.76	368.4	0.199	0.08
3	399.26	96.501	0.919	408.91	385.76	0.319	0.054
4	420.48	96.293	1.107	432.05	408.91	0.332	0.067
5	524.64	98.26	0.337	530.42	487.99	0.172	0.019
6	551.64	98.043	0.201	563.21	530.42	0.263	0.015
7	651.94	98.14	0.659	655.8	628.79	0.113	0.03
8	673.16	96.716	1.493	682.8	655.8	0.316	0.114
9	758.02	96.362	0.691	767.67	707.88	0.589	0.101
10	813.96	94.502	1.597	839.03	767.67	1.451	0.252
11	866.04	94.639	2.214	943.19	840.96	1.347	0.379
12	1022.27	95.126	4.847	1055.06	954.76	1.035	1.009
13	1203.58	88.515	11.223	1334.74	1056.99	8.314	8
14	1369.46	97.609	2.066	1390.68	1348.24	0.256	0.197
15	1435.04	93.878	1.331	1442.75	1390.68	0.793	0.167
16	1452.4	94.133	1.646	1477.47	1444.68	0.509	0.112
17	1516.05	92.071	1.055	1519.91	1485.19	0.643	0.075
18	1597.06	66.218	21.099	1666.5	1519.91	17.657	9.156
19	1691.57	80.578	6.554	1761.01	1668.43	4.934	1.17
20	1801.51	99.381	0.116	1803.44	1784.15	0.031	0.01
21	1867.09	99.365	0.608	1880.6	1855.52	0.041	0.038
22	2335.8	83.248	3.257	2343.51	2277.93	2.539	0.34
23	2360.87	78.033	11.613	2393.66	2345.44	2.853	1.099
24	2858.51	97.124	0.539	2877.79	2752.42	0.734	0.078
	320.23	95.695	2.49	2991.59	2879.72	1.321	0.591
	3414	78.405	0.264	3433.29	3406.29	2.827	0.026
	3587.6	88.098	0.458	3603.03	3579.88	1.243	0.024
	3739.97	96.78	0.702	3763.12	3734.19	0.28	0.054



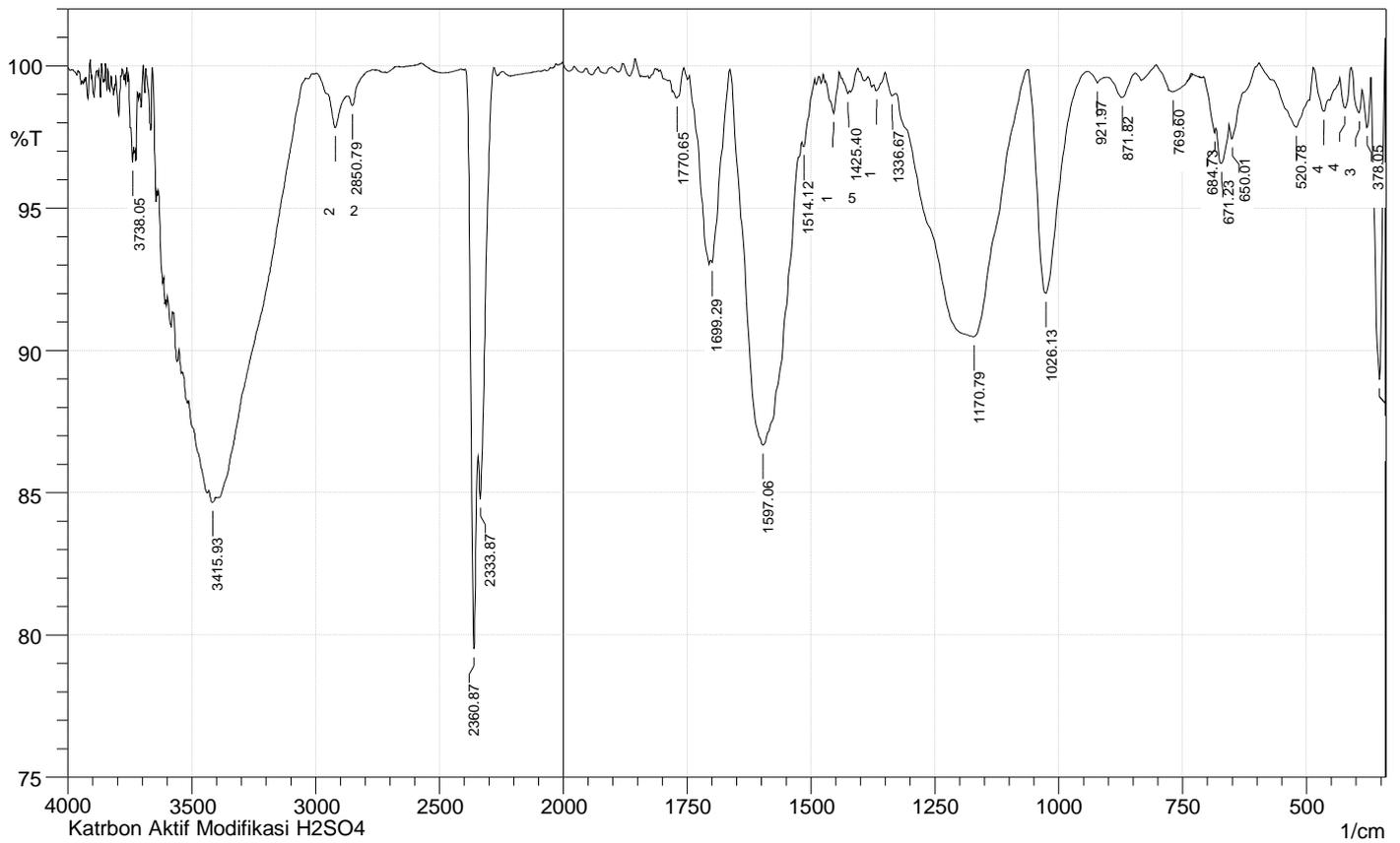
Lampiran 5. Spektrum FTIR dari KATK



No.	Peak	Intensity	Corr. Intensity	Base (H)	Base (L)	Area	Corr. Area
1	352.97	86.891	12.192	368.4	343.33	0.906	0.81
2	378.05	97.962	1.446	387.69	370.33	0.118	0.067
3	424.34	97.733	0.568	432.05	410.84	0.191	0.036
4	543.93	98.457	1.617	626.87	487.99	0.554	0.605
5	671.23	97.518	1.112	682.8	655.8	0.24	0.082
6	798.53	97.706	2.226	844.82	709.8	0.796	0.747
7	873.75	98.858	1.062	906.54	846.75	0.162	0.139
8	925.83	98.763	1.104	950.91	906.54	0.1	0.075
9	1022.27	96.644	3.233	1066.64	962.48	0.703	0.645
10	1120.64	98.384	1.658	1139.93	1068.56	0.246	0.247
11	1161.15	99.204	0.731	1180.44	1139.93	0.081	0.071
12	1261.45	96.383	3.469	1300.02	1180.44	1.246	1.161
13	1377.17	88.572	7.66	1417.68	1300.02	3.18	1.655
14	1425.4	94.405	0.149	1442.75	1423.47	0.434	0.015
15	1452.4	95.706	0.586	1477.47	1448.54	0.298	0.025
16	1585.49	60.139	39.601	1745.58	1477.47	30.683	30.299
17	1813.09	98.97	0.159	1815.02	1801.51	0.032	0.002
18	1863.24	99.396	0.475	1880.6	1855.52	0.043	0.034
19	2333.87	88.878	2.796	2343.51	2279.86	1.543	0.251
20	2360.87	85.161	8.297	2391.73	2345.44	1.767	0.713
21	2856.58	98.299	0.623	2881.65	2792.93	0.359	0.066
22	2922.16	96.871	2.174	2991.59	2881.65	0.862	0.49
23	3412.08	67.87	0.532	3577.95	3406.29	23.37	1.483
24	3726.47	97.027	0.806	3730.33	3718.76	0.115	0.017



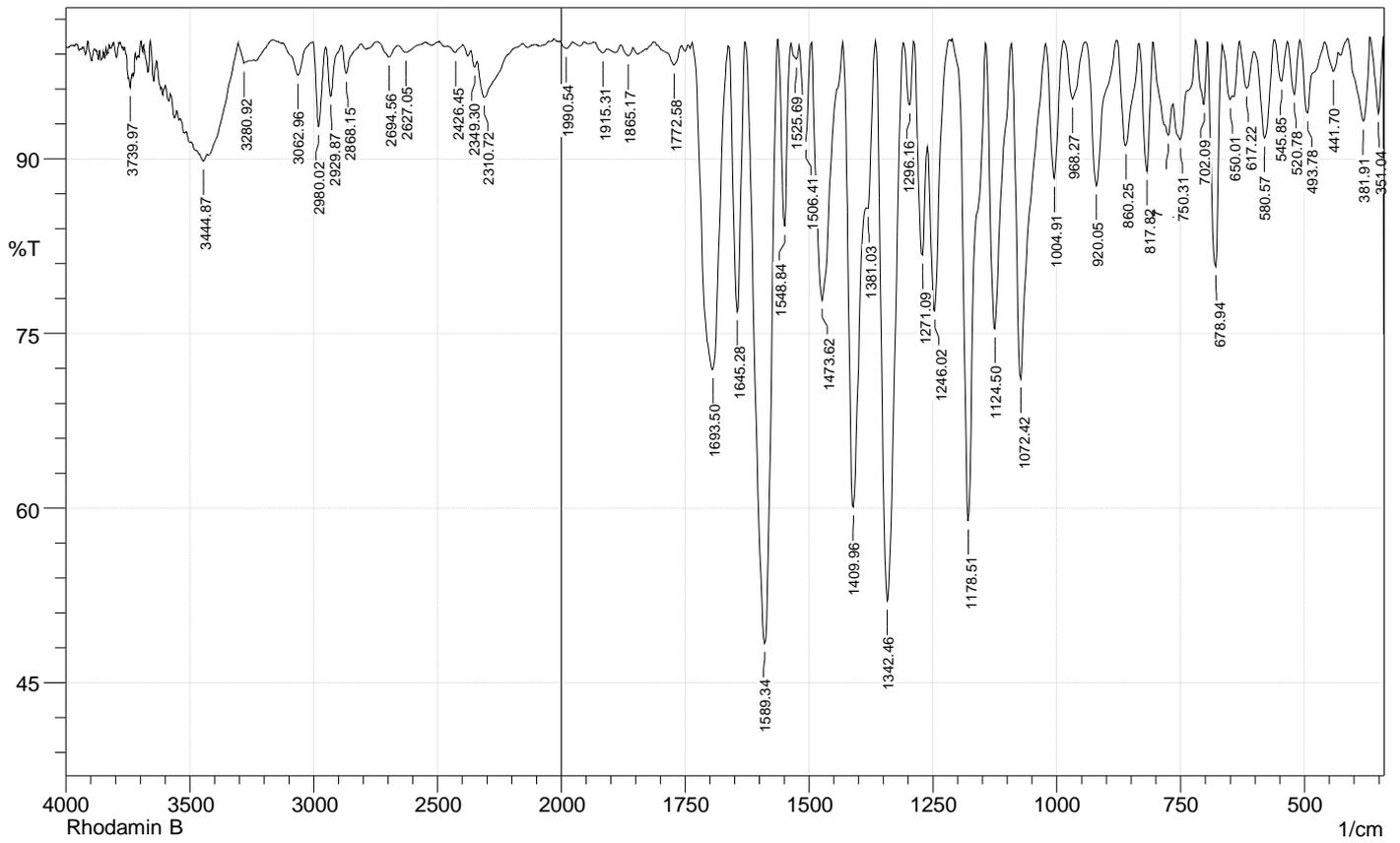
Lampiran 6. Spektrum FTIR dari KAM



No.	Peak	Intensity	Corr. Intensity	Base (H)	Base (L)	Area	Corr. Area
1	352.97	88.965	10.206	368.4	343.33	0.793	0.7
2	378.05	97.833	1.565	387.69	370.33	0.117	0.069
3	393.48	98.358	1.005	408.91	387.69	0.105	0.063
4	422.41	98.526	1.206	432.05	408.91	0.097	0.073
5	464.84	98.404	0.764	486.06	455.2	0.142	0.058
6	520.78	97.848	2.151	596	486.06	0.522	0.536
7	650.01	97.432	0.716	655.8	596	0.288	0.031
8	671.23	96.572	1.294	682.8	655.8	0.347	0.095
9	684.73	97.646	0.306	707.88	682.8	0.15	0.01
10	769.6	99.095	0.806	802.39	732.95	0.179	0.147
11	871.82	98.89	0.793	902.69	846.75	0.172	0.093
12	921.97	99.406	0.299	941.26	902.69	0.067	0.017
13	1026.13	92.006	7.842	1060.85	941.26	1.826	1.741
14	1170.79	90.487	9.04	1327.03	1062.78	6.656	6.025
15	1336.67	98.953	0.349	1350.17	1328.95	0.074	0.019
16	1367.53	99.131	0.315	1373.32	1350.17	0.065	0.02
17	1425.4	99.032	0.213	1442.75	1421.54	0.059	0.009
18	1454.33	98.332	1.321	1469.76	1442.75	0.128	0.085
19	1514.12	97.166	0.498	1517.98	1492.9	0.196	0.023
20	1597.06	86.667	12.006	1662.64	1519.91	5.637	4.726
21	1699.29	93.09	0.434	1701.22	1664.57	0.584	0.038
22	1770.65	98.877	0.542	1778.37	1757.15	0.077	0.033
23	2333.87	84.766	3.571	2343.51	2279.86	2.197	0.345
24	2360.87	79.504	11.046	2393.66	2345.44	2.57	0.991
25	2850.79	98.607	0.511	2870.08	2769.78	0.277	0.016
26	2920.23	97.829	1.432	2995.45	2870.08	0.65	0.287
27	3431.36	63	0.276	3431.36	3404.36	1.937	0.024
28	3745.76	14	0.767	3745.76	3734.19	0.144	0.017



Lampiran 7. Spektrum FTIR dari Rhodamin B



No.	Peak	Intensity	Corr. Intensity	Base (H)	Base (L)	Area	Corr. Area
1	351.04	93.89	6.6	368.4	341.4	0.326	0.382
2	381.91	93.258	7.171	412.77	368.4	0.712	0.79
3	441.7	97.509	1.95	459.06	432.05	0.173	0.125
4	493.78	93.948	6.227	509.21	459.06	0.563	0.594
5	520.78	95.543	4.613	534.28	509.21	0.232	0.248
6	545.85	96.678	3.464	561.29	534.28	0.186	0.204
7	580.57	91.775	7.978	601.79	561.29	0.756	0.709
8	617.22	96.082	3.617	630.72	601.79	0.294	0.252
9	650.01	95.075	1.206	665.44	646.15	0.256	0.05
10	678.94	80.749	18.996	694.37	665.44	1.441	1.409
11	702.09	94.686	5.417	719.45	696.3	0.306	0.32
12	750.31	91.641	4.897	765.74	719.45	1.093	0.59
13	775.38	92.026	3.95	806.25	765.74	0.932	0.457
14	817.82	88.936	11.059	833.25	806.25	0.716	0.714
15	860.25	91.135	8.952	879.54	833.25	0.943	0.956
16	920.05	87.693	12.391	941.26	879.54	1.421	1.451
17	968.27	95.144	4.965	985.62	943.19	0.445	0.463
18	1004.91	88.339	11.682	1022.27	985.62	0.916	0.92
19	1072.42	71.084	28.754	1091.71	1024.2	4.262	4.2
20	1124.5	75.395	24.19	1141.86	1093.64	2.965	2.872
21	1178.51	58.896	41.132	1209.37	1143.79	5.238	5.243
22	1246.02	76.922	16.619	1259.52	1217.08	2.236	1.381
23	1271.09	81.725	12.674	1286.52	1261.45	1.406	0.844
24	1296.16	94.648	5.392	1309.67	1288.45	0.257	0.26
25	1342.46	51.991	48.071	1365.6	1309.67	7.587	7.599
26	1381.03	85.735	2.928	1384.89	1365.6	0.737	0.1
27	1409.96	60.099	33.387	1431.18	1384.89	5.452	3.848
28	1473.62	77.844	21.976	1494.83	1433.11	3.343	3.271
29	1506.41	91.527	8.339	1519.91	1494.83	0.481	0.465
30	1525.69	98.581	1.208	1535.34	1519.91	0.065	0.053
31	1548.84	84.196	15.906	1562.34	1535.34	0.878	0.89
32	1589.34	48.361	51.428	1627.92	1564.27	9.937	9.888
33	1645.28	76.874	22.943	1660.71	1629.85	1.815	1.793

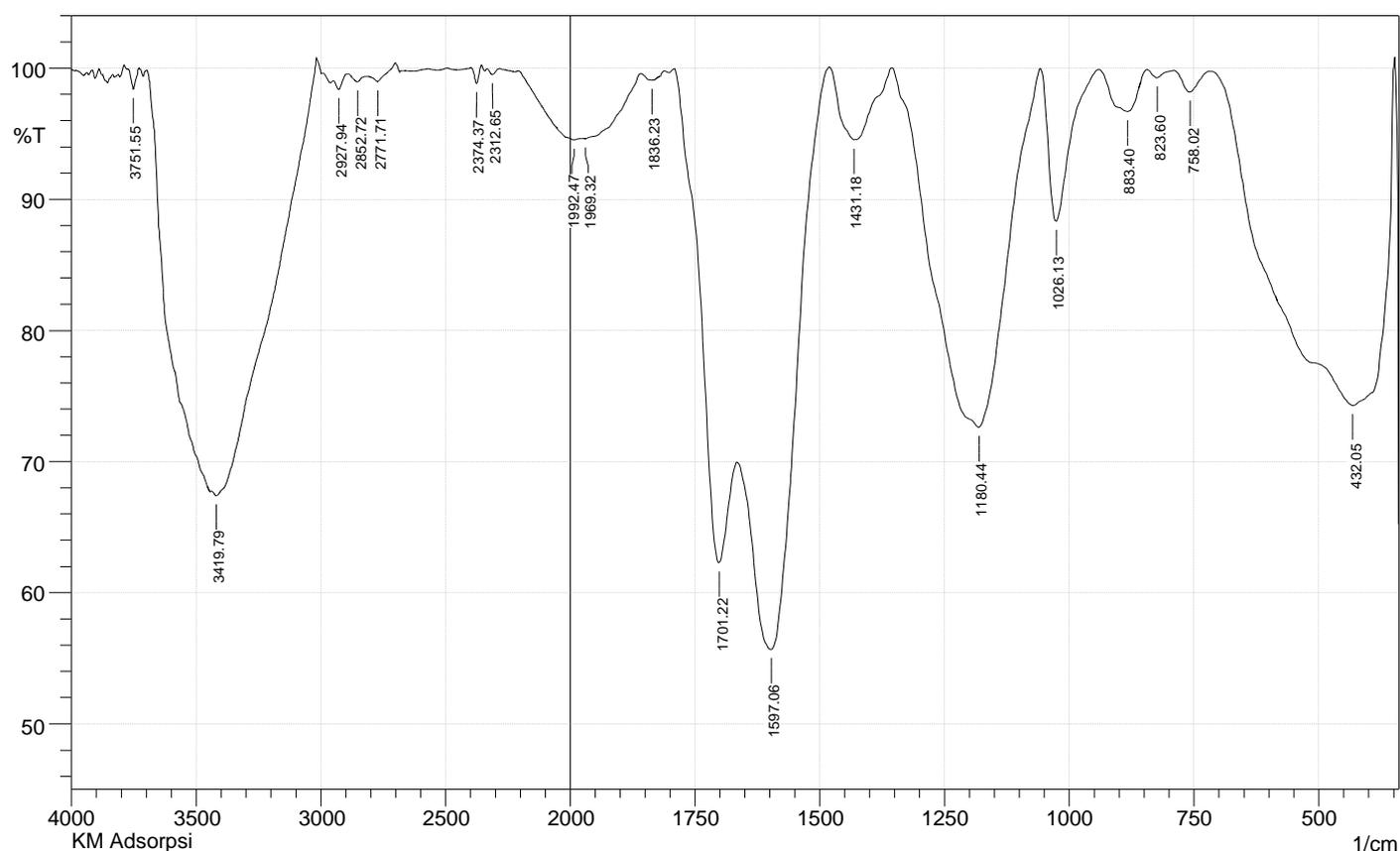
34	1693.5	71.894	27.936	1735.93	1662.64	5.396	5.348
35	1772.58	98.049	1.761	1813.09	1757.15	0.216	0.187
36	1865.17	98.857	0.799	1880.6	1855.52	0.085	0.05
37	1915.31	99.113	0.493	1934.6	1907.6	0.062	0.031
38	1990.54	99.497	0.592	2004.04	1977.04	0.03	0.041
39	2310.72	95.289	3.277	2337.72	2156.42	1.785	1.089
40	2349.3	97.882	0.86	2364.73	2339.65	0.182	0.056
41	2426.45	99.133	0.608	2457.31	2397.52	0.142	0.074
42	2627.05	99.159	0.656	2657.91	2547.97	0.209	0.15
43	2694.56	98.748	1.122	2746.63	2657.91	0.225	0.186
44	2868.15	97.364	2.429	2887.44	2808.36	0.381	0.321
45	2929.87	95.376	4.278	2951.09	2887.44	0.545	0.456
46	2980.02	92.775	7.084	3003.17	2951.09	0.81	0.772
47	3062.96	97.196	2.772	3124.68	3008.95	0.579	0.563
48	3280.92	98.219	0.94	3305.99	3257.77	0.258	0.087
49	3444.87	89.825	0.67	3473.8	3431.36	1.897	0.068
50	3739.97	96.149	0.913	3745.76	3734.19	0.171	0.021

Com
Rhod



Resolution;
Apodization;
User; Kimia Terpadu

Lampiran 8. Spektrum FTIR dari KAM setelah Adsorpsi



No.	Peak	Intensity	Corr. Intensity	Base (H)	Base (L)	Area	Corr. Area
1	432.05	74.281	25.746	713.66	349.12	30.737	30.632
2	758.02	98.17	1.614	790.81	719.45	0.304	0.236
3	823.6	99.275	0.588	844.82	790.81	0.095	0.061
4	883.4	96.688	3.211	941.26	844.82	0.837	0.795
5	1026.13	88.323	11.632	1056.99	941.26	2.495	2.464
6	1180.44	72.598	27.375	1354.03	1058.92	21.368	21.34
7	1431.18	94.54	5.53	1479.4	1355.96	1.716	1.748
8	1597.06	55.668	25.379	1664.57	1481.33	26.639	12.683
9	1701.22	62.283	16.086	1789.94	1666.5	14.088	4.364
10	1836.23	99.08	0.6	1859.38	1811.16	0.141	0.075
11	1969.32	94.616	0.258	1975.11	1859.38	1.892	0.42
12	1992.47	94.532	0.442	2206.57	1977.04	3.396	0.518
13	2312.65	99.518	0.437	2331.94	2279.86	0.058	0.048
14	2374.37	98.843	1.294	2397.52	2355.08	0.085	0.108
15	2771.71	98.964	0.788	2814.14	2700.34	0.257	0.198
16	2852.72	98.957	0.511	2891.3	2814.14	0.256	0.077
17	2927.94	98.384	0.844	2949.16	2891.3	0.267	0.09
18	3419.79	67.384	1.721	3437.15	3016.67	39.965	5.27
19	3751.55	98.406	1.564	3772.76	3728.4	0.146	0.14

Comment;
KM Adsorpsi

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No. of Scans;

Resolution;

Apodization;



Lampiran 9. Hasil Analisis dengan Metode Titrasi Boehm

V. Sampel (Vs) (mL)	V. Titran NaHCO ₃ (Vp) (mL)	Normal NaHCO ₃	Normal HCl	V. HCl (mL)	Normal NaOH	V. NaOH (mL)	Massa Karbon (g)	n Karboksilat (meq/g)
50	5	0.0503	0.0466	10	0.0573	4.6	0.1008	4,869047619
50	5	0.0503	0.0466	10	0.0573	4.6	0.1008	4,869047619
50	5	0.0503	0.0466	10	0.0573	4.8	0.1008	6,005952381
50	5	0.0503	0.0466	10	0.0573	4.8	0.1008	6,005952381
50	5	0.0503	0.0466	10	0.0573	4.8	0.1008	6,005952381
50	5	0.0503	0.0466	10	0.0573	4.9	0.1008	6,574404762
50	5	0.0503	0.0466	10	0.0573	4.9	0.1008	6,574404762
Rata-Rata								5.763840189

Contoh perhitungan pada n karboksilat karbon aktif

$$n_{\text{karboksilat}} = \frac{V_{\text{NaHCO}_3} N_{\text{NaHCO}_3} - (N_{\text{HCl}} V_{\text{HCl}} - N_{\text{NaOH}} V_{\text{NaOH}}) \frac{V_p}{V_s}}{w}$$

$$n_{\text{karboksilat}} = \frac{[5 \times 0.0503 - (0.0466 \times 10 - 0.0573 \times 4.6)] \frac{50}{5}}{0.1008}$$

$$n_{\text{karboksilat}} = 4.869047619$$

V. Sampel (Vs) (mL)	V. Titran Na ₂ CO ₃ (Vp)	Normal Na ₂ CO ₃	Normal HCl	V. HCl (mL)	Normal NaOH	V. NaOH (mL)	Massa Karbon (g)	n Lakton (meq/g)
50	5	0.05014	0.0466	10	0.0573	4.8	0.1026	0,953564467
50	5	0.05014	0.0466	10	0.0573	4.8	0.1026	0,953564467
50	5	0.05014	0.0466	10	0.0573	4.8	0.1026	-0,183340295
50	5	0.05014	0.0466	10	0.0573	4.8	0.1026	-0,183340295
50	5	0.05014	0.0466	10	0.0573	4.9	0.1026	0,375139237
50	5	0.05014	0.0466	10	0.0573	4.8	0.1026	-0,751792676
50	5	0.05014	0.0466	10	0.0573	4.9	0.1026	-0,193313144
Rata-Rata								0.272906575

Contoh perhitungan pada n Lakton karbon aktif

$$n_{\text{lakton}} = \frac{V_{\text{Na}_2\text{CO}_3} N_{\text{Na}_2\text{CO}_3} - (N_{\text{HCl}} V_{\text{HCl}} - N_{\text{NaOH}} V_{\text{NaOH}}) \frac{V_p}{V_s}}{w} - n_{\text{karboksilat}}$$

$$= \frac{5 \times 0.05014 - (0.0466 \times 10 - 0.0573 \times 4.8) \frac{50}{5}}{0.1026} - 5.763840189$$

$$= 0.953564467$$



V. Sampel (Vs) (mL)	V. Titran NaOH (Vp) (mL)	Normal NaOH	Normal HCl	V. HCl (mL)	Normal NaOH	V. NaOH (mL)	Massa Karbon (g)	n Lakton (meq/g)
50	5	0.0573	0.0466	10	0.0573	4.1	0.1017	-0,372267936
50	5	0.0573	0.0466	10	0.0573	4.2	0.1017	0,191153893
50	5	0.0573	0.0466	10	0.0573	4.4	0.1017	1,31799755
50	5	0.0573	0.0466	10	0.0573	4.3	0.1017	0,754575722
50	5	0.0573	0.0466	10	0.0573	4.4	0.1017	0,759518018
50	5	0.0573	0.0466	10	0.0573	4.2	0.1017	0,191153893
50	5	0.0573	0.0466	10	0.0573	4.4	0.1017	0,759518018
Rata-Rata								0.387294347

Contoh perhitungan pada n fenol karbon aktif

$$n_{\text{phenolic}} = \frac{[V_{\text{NaOH}} N_{\text{NaOH}} - (N_{\text{HCl}} V_{\text{HCl}} - N_{\text{NaOH}} V_{\text{NaOH}})] \frac{V_p}{V_s}}{w} - n_{\text{carboxylic}} - n_{\text{lactonic}}$$

$$n_{\text{lakton}} = \frac{5 \times 0.0573 - (0.0466 \times 10 - 0.0573 \times 4.2) \frac{50}{5}}{0.1009} - 5.763840189 - 0.272906575$$

$$n_{\text{lakton}} = 0.158284922$$

V. Sampel (Vs) (mL)	V. Titran NaOH (Vp) (mL)	Normal HCl	Normal NaOH	V. NaOH (mL)	Normal HCl	V. HCl (mL)	Massa Karbon (g)	n Lakton (meq/g)
50	5	0.0466	0.0573	7.5	0.0466	4.3	0.1055	0,344075829
50	5	0.0466	0.0573	7.5	0.0466	4.2	0.1055	-0,097630332
50	5	0.0466	0.0573	7.5	0.0466	4.2	0.1055	-0,097630332
50	5	0.0466	0.0573	7.5	0.0466	4.3	0.1055	0,344075829
50	5	0.0466	0.0573	7.5	0.0466	4.2	0.1055	-0,097630332
50	5	0.0466	0.0573	7.5	0.0466	4.2	0.1055	-0,097630332
Rata-Rata								0.050137454

Contoh perhitungan pada n Basa Total karbon aktif

$$n_{\text{total basa}} = \frac{[V_{\text{HCl}} N_{\text{HCl}} - (N_{\text{NaOH}} V_{\text{NaOH}} - N_{\text{HCl}} V_{\text{HCl}})] \frac{V_p}{V_s}}{w}$$

$$= \frac{[5 \times 0.0466 - (0.0573 \times 7.5 - 0.0466 \times 4.3) \frac{50}{5}]}{0.1055}$$

$$= 0.344075829$$



V. Sampel (Vs) (mL)	V. Titran NaHCO ₃ (Vp) (mL)	Normal NaHCO ₃	Normal HCl	V. HCl (mL)	Normal NaOH	V. NaOH (mL)	Massa Karbon (g)	n Karboksilat (meq/g)
50	5	0,0503	0,053	7	0,0462	8,4	0,1002	26,80439122
50	5	0,0503	0,053	7	0,0462	8,1	0,1002	25,42115768
50	5	0,0503	0,053	7	0,0462	7,9	0,1002	24,499002
50	5	0,0503	0,053	7	0,0462	8,4	0,1002	26,80439122
50	5	0,0503	0,053	7	0,0462	8,5	0,1002	27,26546906
50	5	0,0503	0,053	7	0,0462	8,4	0,1002	26,80439122
Rata-Rata								26,26646707

Contoh perhitungan pada n karboksilat karbon aktif termodifikasi

$$n_{\text{karboksilat}} = \frac{V_{\text{NaHCO}_3} N_{\text{NaHCO}_3} - (N_{\text{HCl}} V_{\text{HCl}} - N_{\text{NaOH}} V_{\text{NaOH}}) \frac{V_p}{V_s}}{w}$$

$$n_{\text{karboksilat}} = \frac{[5 \times 0.0503 - (0.053 \times 7 - 0.0462 \times 8,4)] \frac{50}{5}}{0.1002}$$

$$n_{\text{karboksilat}} = 26.80439122$$

V. Sampel (Vs) (mL)	V. Titran Na ₂ CO ₃ (Vp) (mL)	Normal Na ₂ CO ₃	Normal HCl	V. HCl (mL)	Normal NaOH	V. NaOH (mL)	Massa Karbon (g)	n Lakton (meq/g)
50	5	0,0503	0,053	7	0,0462	3,6	0,1002	-22,13173653
50	5	0,0503	0,053	7	0,0462	3,9	0,1002	-19,36526946
50	5	0,0503	0,053	7	0,0462	3,6	0,1002	-19,82634731
50	5	0,0503	0,053	7	0,0462	3,2	0,1002	-23,9760479
50	5	0,0503	0,053	7	0,0462	3,2	0,1002	-24,43712575
50	5	0,0503	0,053	7	0,0462	3,9	0,1002	-20,74850299
Rata-Rata								-21,74750499

Contoh perhitungan pada n Lakton karbon aktif termodifikasi

$$n_{\text{lakton}} = \frac{V_{\text{Na}_2\text{CO}_3} N_{\text{Na}_2\text{CO}_3} - (N_{\text{HCl}} V_{\text{HCl}} - N_{\text{NaOH}} V_{\text{NaOH}}) \frac{V_p}{V_s}}{w} - n_{\text{karboksilat}}$$

$$= \frac{5 \times 0.0503 - (0.053 \times 7 - 0.0462 \times 3,6) \frac{50}{5}}{0.1002} - 26.26646707$$

$$= -22,13173653$$



V. Sampel (Vs) (mL)	V. Titran NaOH (Vp) (mL)	Normal NaOH	Normal HCl	V. HCl (mL)	Normal NaOH	V. NaOH (mL)	Massa Karbon (g)	n Lakton (meq/g)
50	5	0,0462	0,053	7	0,0462	8	0,1010	18,06001858
50	5	0,0462	0,053	7	0,0462	8,5	0,1010	18,96391376
50	5	0,0462	0,053	7	0,0462	8,4	0,1010	19,88972155
50	5	0,0462	0,053	7	0,0462	8,8	0,1010	23,56373589
50	5	0,0462	0,053	7	0,0462	8,6	0,1010	22,64888441
50	5	0,0462	0,053	7	0,0462	8,5	0,1010	18,96391376
Rata-Rata								20,34836466

Contoh perhitungan pada n fenol

$$n_{\text{phenolic}} = \frac{[V_{\text{NaOH}}N_{\text{NaOH}} - (N_{\text{HCl}}V_{\text{HCl}} - N_{\text{NaOH}}V_{\text{NaOH}})] \frac{V_p}{V_s}}{w} - n_{\text{carboxylic}} - n_{\text{lactonic}}$$

$$n_{\text{lakton}} = \frac{5 \times 0,0462 - (0,053 \times 7 - 0,0462 \times 8) \frac{50}{5}}{0,1010} - 26,26646707 + 21,74750499$$

$$n_{\text{lakton}} = 18,06001858$$

V. Sampel (Vs) (mL)	V. Titran NaOH (Vp) (mL)	Normal HCl	Normal NaOH	V. NaOH (mL)	Normal HCl	V. HCl (mL)	Massa Karbon (g)	n Lakton (meq/g)
50	5	0,053	0,0462	10	0,053	3,75	0,1007	0,173783515
50	5	0,053	0,0462	10	0,053	3,6	0,1007	-0,615690169
50	5	0,053	0,0462	10	0,053	3,7	0,1007	-0,089374379
50	5	0,053	0,0462	10	0,053	3,8	0,1007	0,43694141
50	5	0,053	0,0462	10	0,053	3,77	0,1007	0,279046673
50	5	0,053	0,0462	10	0,053	3,7	0,1007	-0,089374379
Rata-Rata								0,015888779

Contoh perhitungan pada n basa total

$$n_{\text{total basa}} = \frac{[V_{\text{HCl}}N_{\text{HCl}} - (N_{\text{NaOH}}V_{\text{NaOH}} - N_{\text{HCl}}V_{\text{HCl}})] \frac{V_p}{V_s}}{w}$$

$$n_{\text{total basa}} = \frac{[5 \times 0,053 - (0,0462 \times 10 - 0,053 \times 3,75)] \frac{50}{5}}{0,1007}$$

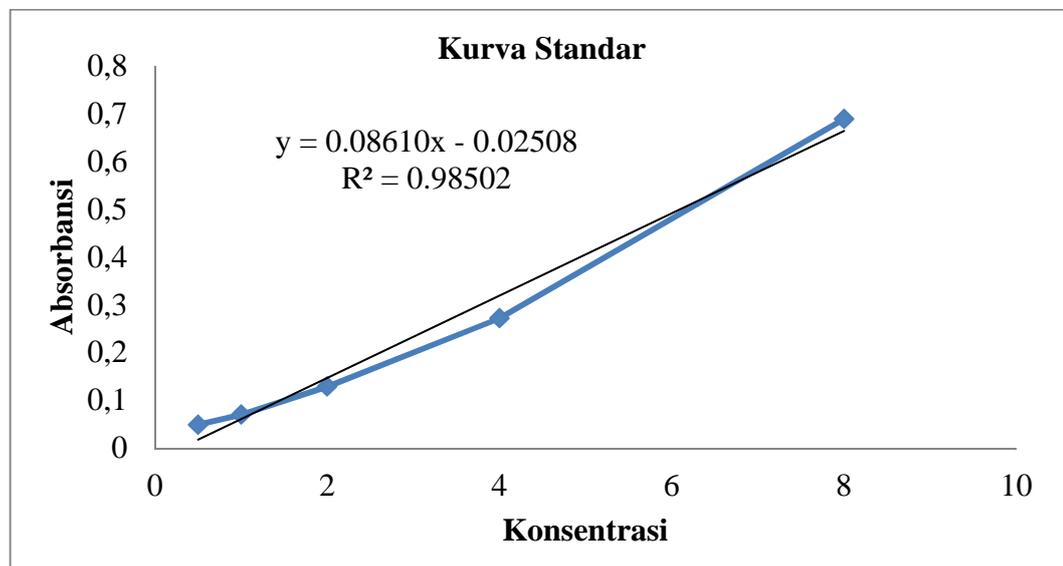
$$= 0,173783515$$



Lampiran 10. Penentuan Luas Permukaan dengan Metilen Biru

Standar Metilen Biru

Konsentrasi	Absorbansi
0.5	0.049
1	0.07
2	0.129
4	0.272
8	0.689



Data Penentuan Luas Permukaan Karbon Aktif dari Tempurung Kluwak

Absorbansi	C_0 (mg/L)	FP	C_e (mg/L)	W_a (g)	q_e (mg/g)	S (m ² /g)
1,74	1933,8908	50	1010,7443	0,3019	76,4447	278,4934
0.236	1933,8908		3,0323	0.3034	159,1017	588,7211
1.68	2349.686	50	975,9010	0.3042	78,7303	286,9836



$$q = \frac{(C_0 - C)V}{W}$$

Contoh perhitungan jumlah metilen biru yang diadsorpsi (q_e) pada:

$$q_e = \frac{(1933,8908 - 3.0323) \frac{\text{mg}}{\text{L}}}{0.3034 \text{ g}} \times 0,025 \text{ L}$$

$$= 159,1017 \text{ mg/g}$$

$$S = \frac{X_m \cdot N \cdot a}{Mr}$$

Contoh perhitungan luas permukaan adsorben (S) pada:

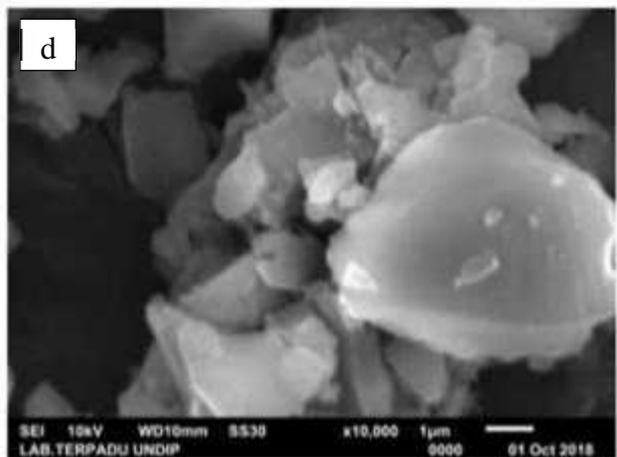
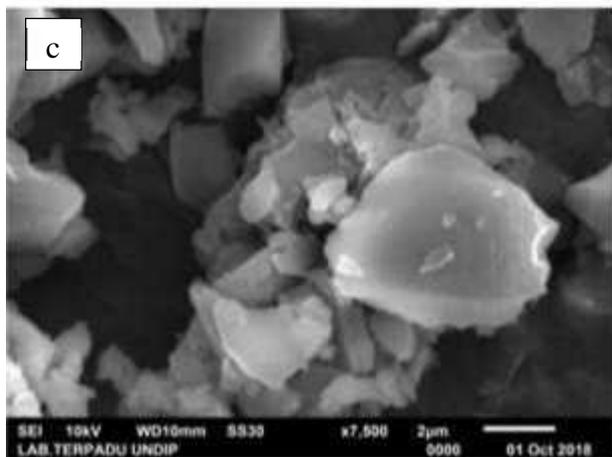
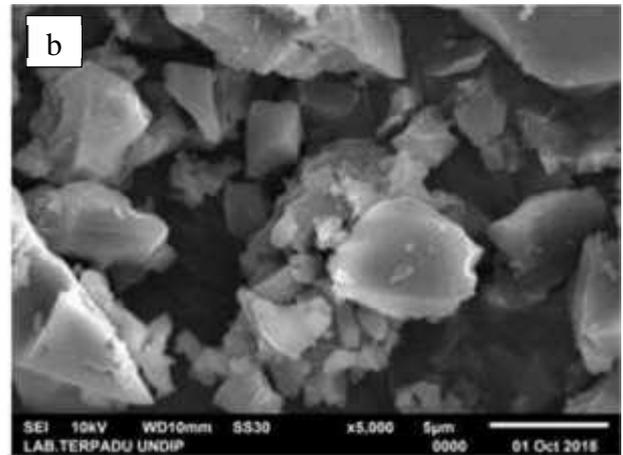
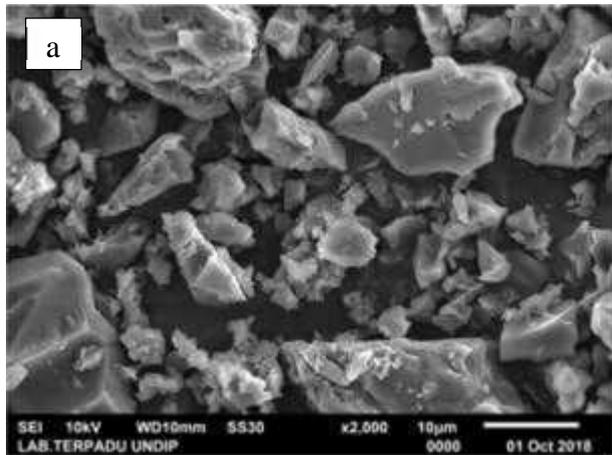
$$S = \frac{(159,1017 \times 6,02 \times 197)}{320,5 \text{ g/mol}}$$

$$= 588,7211 \text{ (m}^2\text{/g)}.$$



Lampiran 11. Analisis dengan Metode SEM

a. Karbon Aktif Tempurung Kluwak

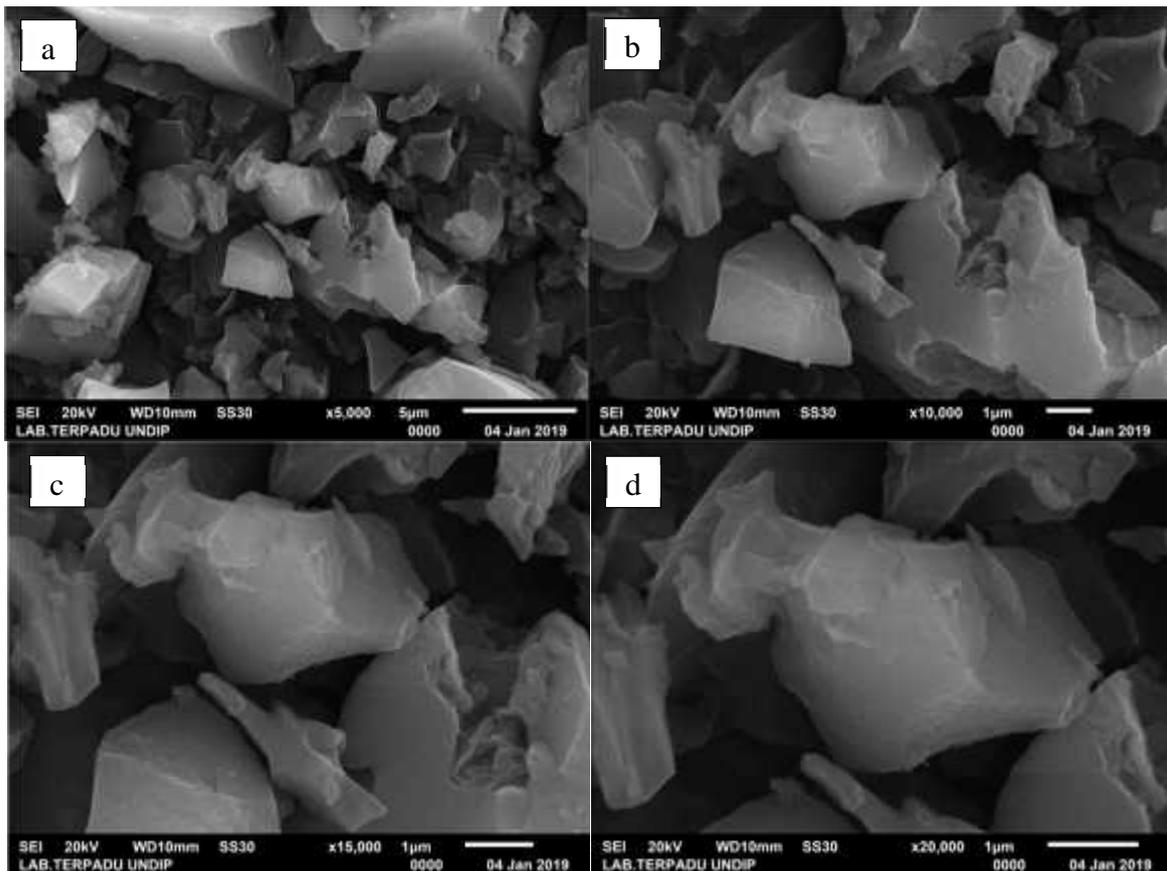


Keterangan:

- a : perbesaran 2000 kali
- b : perbesaran 5000 kali
- c : perbesaran 7500 kali
- d : perbesaran 10000 kali



b. Karbon Aktif Termodifikasi H_2SO_4

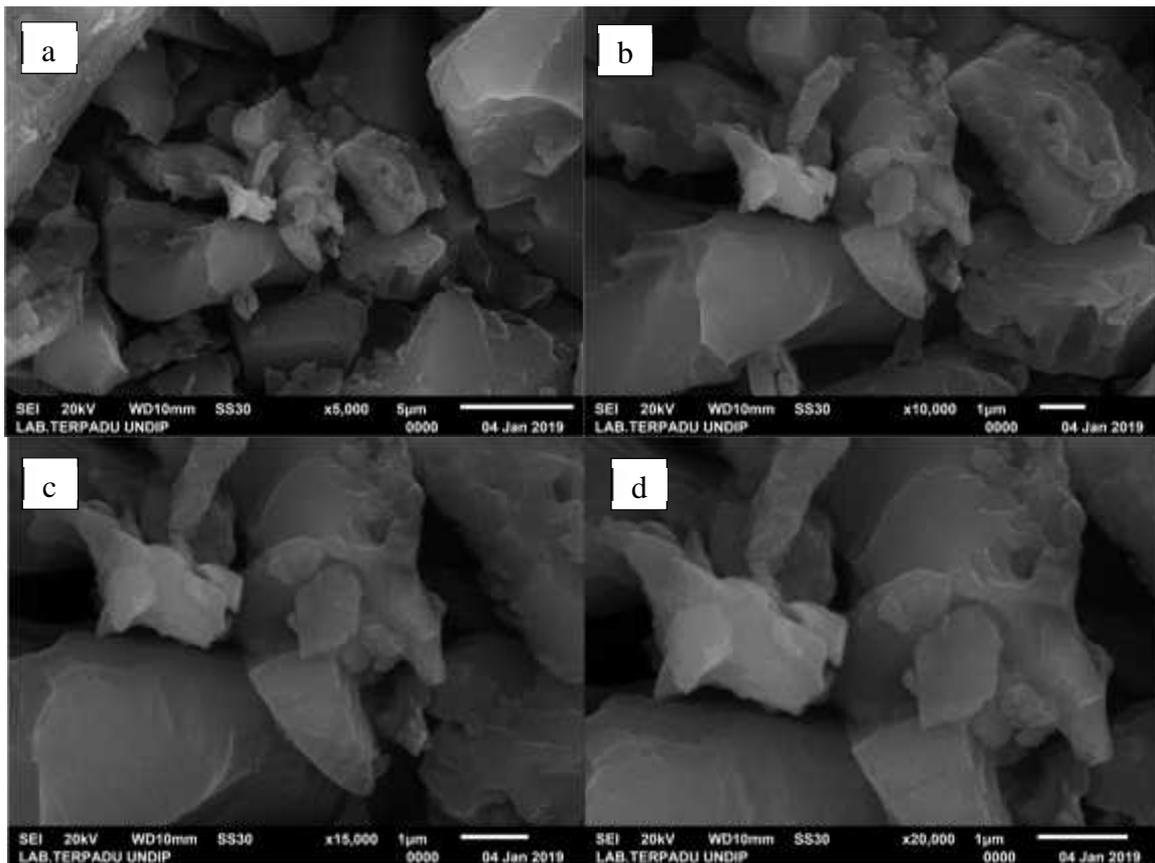


Keterangan:

- a : perbesaran 5000 kali
- b : perbesaran 10000 kali
- c : perbesaran 15000 kali
- d : perbesaran 20000 kali



c. Karbon sesudah Adsorpsi



Keterangan:

- a : perbesaran 5000 kali
- b : perbesaran 10000 kali
- c : perbesaran 15000 kali
- d : perbesaran 20000 kali



Lampiran 12. Hasil Analisis BET

Quantachrome NovaWin - Data Acquisition and Reduction for NOVA instruments

©1994-2010, Quantachrome Instruments
version 11.0



Analysis

Operator:nova
Sample ID: KTK
Sample Desc:
Sample weight: 0.1355 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 481.8 min
Cell ID: 62

Date:2018/09/20

Filename:
Comment:
Sample Volume: 0.03474 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:03:11

Report

Operator:nova
Date:9/24/2018

Sample Density: 3.9 g/cc

Equil timeout: 240/240 sec (ads/des)

Instrument: Nova Station A
F/W version: 0.00

BJH Pore Size Distribution Adsorption

Data Reduction Parameters Data

t-Method	Calc. method: de Boer	Ignoring P-tags below 0.35 P/Po
BJH/DH method	Moving pt. avg.: off	Temperature 77.350K
Adsorbate	Nitrogen	Cross Section: 16.200 Å ²
	Molec. Wt.: 28.013 g	Liquid Density: 0.808 g/cc
	Contact Angle: 0.0 degrees	Surf. Tension: 8.850 erg/cm ²

BJH Pore Size Distribution Adsorption Data

Diameter	Pore Volume	Pore Surf Area	dV(d)	dS(d)	dV(logd)	dS(logd)
[Å]	[cc/g]	[m ² /g]	[cc/Å/g]	[m ² /Å/g]	[cc/g]	[cc/g]
31.4480	5.0660e-04	6.4436e-01	2.2609e-04	2.8757e-01	1.6365e-02	2.0815e+01
33.7029	1.3172e-03	1.6064e+00	3.5722e-04	4.2396e-01	2.7711e-02	3.2888e+01
35.9895	2.2228e-03	2.6129e+00	3.9307e-04	4.3688e-01	3.2563e-02	3.6191e+01
38.5117	3.2606e-03	3.6909e+00	3.7872e-04	3.9336e-01	3.3569e-02	3.4867e+01
41.6063	4.4991e-03	4.8815e+00	3.5910e-04	3.4523e-01	3.4382e-02	3.3055e+01
44.9633	5.6870e-03	5.9383e+00	3.6382e-04	3.2366e-01	3.7651e-02	3.3495e+01
48.7264	6.9650e-03	6.9874e+00	2.9991e-04	2.4620e-01	3.3628e-02	2.7605e+01
53.3936	8.7364e-03	8.3145e+00	3.4918e-04	2.6159e-01	4.2897e-02	3.2136e+01
58.5965	1.0092e-02	9.2396e+00	2.5413e-04	1.7348e-01	3.4264e-02	2.3390e+01
64.1588	1.1733e-02	1.0263e+01	2.8347e-04	1.7673e-01	4.1849e-02	2.6091e+01
71.1457	1.3209e-02	1.1093e+01	1.8038e-04	1.0141e-01	2.9517e-02	1.6595e+01
80.1906	1.4741e-02	1.1857e+01	1.5456e-04	7.7096e-02	2.8502e-02	1.4217e+01
91.8973	1.7131e-02	1.2897e+01	1.7698e-04	7.7032e-02	3.7381e-02	1.6271e+01
103.8269	1.8801e-02	1.3541e+01	1.6131e-04	6.2144e-02	3.8531e-02	1.4844e+01
117.8947	2.0398e-02	1.4083e+01	8.9828e-05	3.0477e-02	2.4339e-02	8.2578e+00
143.7227	2.2192e-02	1.4582e+01	5.2965e-05	1.4741e-02	1.7446e-02	4.8556e+00
188.1612	2.3910e-02	1.4947e+01	3.1227e-05	6.6383e-03	1.3432e-02	2.8555e+00
258.3460	2.6221e-02	1.5305e+01	2.7068e-05	4.1910e-03	1.5954e-02	2.4702e+00
428.0373	2.9250e-02	1.5588e+01	1.1927e-05	1.1145e-03	1.1401e-02	1.0654e+00
1231.3583	3.3423e-02	1.5723e+01	3.0847e-06	1.0020e-04	7.7818e-03	2.5279e-01

BJH adsorption summary

Surface Area = 15.723 m²/g
Pore Volume = 0.033 cc/g
Pore Diameter Dv(d) = 35.990 Å



Optimization Software:
www.balesio.com



Analysis

Operator:nova
Sample ID: KATK
Sample Desc:
Sample weight: 0.1046 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 485.6 min
Cell ID: 32

Date:2018/09/20

Filename: C:\QCdata\Physisorb\KATK.qps
Comment:
Sample Volume: 0.02682 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:06:55

Report

Operator:nova
Date:9/24/2018
Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station B
F/W version: 0.00

BJH Pore Size Distribution Adsorption

Data Reduction Parameters Data

t-Method	Calc. method: de Boer	Ignoring P-tags below 0.35 P/Po
BJH/DH method	Moving pt. avg.: off	Temperature 77.350K
Adsorbate	Nitrogen	Cross Section: 16.200 Å²
	Molec. Wt.: 28.013 g	Liquid Density: 0.808 g/cc
	Contact Angle: 0.0 degrees	Surf. Tension: 8.850 erg/cm²

BJH Pore Size Distribution Adsorption Data

Diameter [Å]	Pore Volume [cc/g]	Pore Surf Area [m²/g]	dV(d) [cc/Å/g]	dS(d) [m²/Å/g]	dV(logd) [cc/g]	dS(logd) [cc/g]
31.5838	3.5766e-04	4.5296e-01	1.5483e-04	1.9609e-01	1.1255e-02	1.4254e+01
33.7806	1.0030e-03	1.2171e+00	3.0972e-04	3.6674e-01	2.4083e-02	2.8517e+01
35.8909	1.6931e-03	1.9862e+00	3.2289e-04	3.5986e-01	2.6677e-02	2.9731e+01
38.6911	2.8301e-03	3.1617e+00	3.2832e-04	3.3942e-01	2.9230e-02	3.0219e+01
42.0003	4.2172e-03	4.4827e+00	4.3962e-04	4.1868e-01	4.2495e-02	4.0471e+01
45.2493	4.9130e-03	5.0978e+00	2.0818e-04	1.8403e-01	2.1680e-02	1.9165e+01
49.1325	6.6756e-03	6.5328e+00	3.9845e-04	3.2439e-01	4.5047e-02	3.6674e+01
53.6435	7.8476e-03	7.4067e+00	2.5486e-04	1.9004e-01	3.1461e-02	2.3459e+01
58.6399	9.2071e-03	8.3341e+00	2.5202e-04	1.7191e-01	3.4004e-02	2.3195e+01
64.5853	1.0573e-02	9.1797e+00	2.1019e-04	1.3018e-01	3.1232e-02	1.9343e+01
71.5708	1.1783e-02	9.8564e+00	1.6197e-04	9.0524e-02	2.6668e-02	1.4905e+01
80.0508	1.3356e-02	1.0642e+01	1.6577e-04	8.2830e-02	3.0519e-02	1.5250e+01
91.7744	1.4946e-02	1.1335e+01	1.1393e-04	4.9657e-02	2.4029e-02	1.0473e+01
104.8761	1.6272e-02	1.1841e+01	1.0826e-04	4.1292e-02	2.6114e-02	9.9601e+00
120.5241	1.7696e-02	1.2314e+01	7.4777e-05	2.4817e-02	2.0709e-02	6.8729e+00
149.2373	1.9476e-02	1.2791e+01	4.6379e-05	1.2431e-02	1.5849e-02	4.2480e+00
192.2098	2.1344e-02	1.3179e+01	3.9265e-05	8.1713e-03	1.7289e-02	3.5979e+00
254.7244	2.2907e-02	1.3425e+01	2.0176e-05	3.1683e-03	1.1742e-02	1.8439e+00
409.8326	2.5141e-02	1.3643e+01	9.6001e-06	9.3698e-04	8.8104e-03	8.5990e-01
1007.1011	2.8420e-02	1.3773e+01	3.4086e-06	1.3538e-04	7.2618e-03	2.8842e-01

BJH adsorption summary

Surface Area = 13.773 m²/g
Pore Volume = 0.028 cc/g
Pore Diameter Dv(d) = 42.000 Å





Analysis

Operator:nova
Sample ID: KTM-H2SO4
Sample Desc:
Sample weight: 0.1708 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 490.3 min
Cell ID: 92

Date:2018/09/20

Filename:
Comment:
Sample Volume: 0.0438 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:11:38

Report

Operator:nova
Date:9/24/2018
C:\QCdata\Physisorb\KTM-H2SO4.qps
Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station C
FW version: 0.00

BJHPoreSizeDistribution Adsorption

Data Reduction Parameters Data

t-Method	Calc. method: de Boer		
BJH/DHmethod	Moving pt. avg.: off	Ignoring P-tags below 0.35 P/Po	
Adsorbate	Nitrogen	Temperature 77.350K	
	Molec. Wt.: 28.013 g	Cross Section: 16.200 Å ²	Liquid Density: 0.808 g/cc
	Contact Angle: 0.0 degrees	Surf. Tension: 8.850 erg/cm ²	

BJH Pore Size Distribution Adsorption Data

Diameter	Pore Volume	Pore Surf Area	dV(d)	dS(d)	dV(logd)	dS(logd)
[Å]	[cc/g]	[m ² /g]	[cc/Å/g]	[m ² /Å/g]	[cc/g]	[cc/g]
31.2869	1.4290e-03	1.8270e+00	6.3454e-04	8.1125e-01	4.5693e-02	5.8418e+01
33.4753	3.4862e-03	4.2851e+00	9.6815e-04	1.1569e+00	7.4600e-02	8.9140e+01
35.7002	5.0893e-03	6.0813e+00	6.8955e-04	7.7260e-01	5.6663e-02	6.3487e+01
38.1749	7.1767e-03	8.2685e+00	7.9532e-04	8.3334e-01	6.9882e-02	7.3223e+01
41.2358	9.1203e-03	1.0154e+01	5.5576e-04	5.3911e-01	5.2738e-02	5.1157e+01
44.5283	1.0854e-02	1.1711e+01	5.6152e-04	5.0441e-01	5.7550e-02	5.1697e+01
48.2164	1.3260e-02	1.3707e+01	5.6091e-04	4.6533e-01	6.2233e-02	5.1628e+01
52.9462	1.4947e-02	1.4982e+01	3.2636e-04	2.4656e-01	3.9756e-02	3.0035e+01
57.9360	1.6953e-02	1.6367e+01	4.1725e-04	2.8807e-01	5.5630e-02	3.8408e+01
63.6565	1.8755e-02	1.7499e+01	2.7163e-04	1.7069e-01	3.9778e-02	2.4996e+01
70.7580	2.0446e-02	1.8455e+01	2.2342e-04	1.2630e-01	3.6366e-02	2.0558e+01
77.9949	2.2181e-02	1.9345e+01	2.5120e-04	1.2883e-01	4.5083e-02	2.3121e+01
88.2436	2.4232e-02	2.0274e+01	1.5087e-04	6.8387e-02	3.0594e-02	1.3868e+01
102.0178	2.5848e-02	2.0908e+01	1.1582e-04	4.5413e-02	2.7165e-02	1.0651e+01
118.1231	2.7617e-02	2.1507e+01	9.6932e-05	3.2824e-02	2.6312e-02	8.9099e+00
145.0495	2.9472e-02	2.2019e+01	5.2087e-05	1.4364e-02	1.7309e-02	4.7733e+00
182.0668	3.2882e-02	2.2768e+01	8.8738e-05	1.9496e-02	3.7063e-02	8.1427e+00
245.7430	3.9030e-02	2.3769e+01	6.9138e-05	1.1254e-02	3.8691e-02	6.2978e+00
370.4875	4.1481e-02	2.4033e+01	1.5267e-05	1.6484e-03	1.2818e-02	1.3839e+00
1246.1876	4.6515e-02	2.4195e+01	3.1639e-06	1.0155e-04	7.6725e-03	2.4627e-01

BJH adsorption summary

Surface Area = 24.195 m²/g
Pore Volume = 0.047 cc/g
Pore Diameter Dv(d) = 33.475 Å





Analysis

Operator:nova
Sample ID: KTK
Sample Desc:
Sample weight: 0.1355 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 481.8 min
Cell ID: 62

Date:2018/09/20

Filename: C:\QCdata\Physisorb\KTK.qps
Comment:
Sample Volume: 0.03474 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:03:11

Report

Operator:nova
Date:9/24/2018
Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station A
F/W version: 0.00

BJH Pore Size Distribution Desorption

Data Reduction Parameters Data

t-Method	Calc. method: de Boer	Ignoring P-tags below 0.35 P/Po
BJH/DH method	Moving pt. avg.: off	Temperature 77.350K
Adsorbate	Nitrogen	Cross Section: 16.200 Å²
	Molec. Wt.: 28.013 g	Liquid Density: 0.808 g/cc
	Contact Angle: 0.0 degrees	Surf. Tension: 8.850 erg/cm²

BJH Pore Size Distribution Desorption Data

Diameter	Pore Volume	Pore Surf Area	dV(d)	dS(d)	dV(logd)	dS(logd)
[Å]	[cc/g]	[m²/g]	[cc/Å/g]	[m²/Å/g]	[cc/g]	[cc/g]
35.7508	2.5421e-03	2.8443e+00	4.1209e-04	4.6107e-01	3.3839e-02	3.7861e+01
43.0412	4.9517e-03	5.0836e+00	2.8644e-04	2.6620e-01	2.8297e-02	2.6298e+01
53.0545	7.3817e-03	6.9156e+00	2.0922e-04	1.5774e-01	2.5457e-02	1.9193e+01
67.3547	9.7998e-03	8.3517e+00	1.4236e-04	8.4545e-02	2.1961e-02	1.3042e+01
90.1134	1.2866e-02	9.7126e+00	1.0745e-04	4.7697e-02	2.2109e-02	9.8136e+00
131.9086	1.5495e-02	1.0510e+01	4.7747e-05	1.4479e-02	1.4289e-02	4.3330e+00
281.0287	1.8698e-02	1.0966e+01	1.3171e-05	1.8747e-03	7.9617e-03	1.1332e+00
1155.1452	2.2197e-02	1.1087e+01	2.3250e-06	8.0508e-05	5.1793e-03	1.7935e-01

BJH desorption summary

Surface Area = 11.087 m²/g
Pore Volume = 0.022 cc/g
Pore Diameter Dv(d) = 35.751 Å





Analysis

Operator:nova
Sample ID: KATK
Sample Desc:
Sample weight: 0.1046 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 485.6 min
Cell ID: 32

Date:2018/09/20

Filename: C:\QCdata\Physisorb\KATK.qps
Comment:
Sample Volume: 0.02682 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:06:55

Report

Operator:nova
Date:9/24/2018
Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station B
F/W version: 0.00

BJH Pore Size Distribution Desorption

Data Reduction Parameters Data

t-Method	Calc. method: de Boer		
BJH/DH method	Moving pt. avg.: off	Ignoring P-tags below 0.35 P/Po	
Adsorbate	Nitrogen	Temperature	77.350K
	Molec. Wt.: 28.013 g	Cross Section:	16.200 Å ²
	Contact Angle: 0.0 degrees	Surf. Tension:	8.850 erg/cm ²
		Liquid Density:	0.808 g/cc

BJH Pore Size Distribution Desorption Data

Diameter	Pore Volume	Pore Surf Area	dV(d)	dS(d)	dV(logd)	dS(logd)
[Å]	[cc/g]	[m ² /g]	[cc/Å/g]	[m ² /Å/g]	[cc/g]	[cc/g]
35.8862	2.4050e-03	2.6807e+00	3.7789e-04	4.2121e-01	3.1143e-02	3.4714e+01
43.2639	5.1083e-03	5.1801e+00	3.2216e-04	2.9786e-01	3.1993e-02	2.9579e+01
52.8136	7.3592e-03	6.8848e+00	2.1020e-04	1.5920e-01	2.5474e-02	1.9293e+01
66.4510	9.4238e-03	8.1276e+00	1.2463e-04	7.5019e-02	1.8970e-02	1.1419e+01
88.7357	1.1529e-02	9.0766e+00	7.5173e-05	3.3886e-02	1.5231e-02	6.8659e+00
130.6693	1.3397e-02	9.6484e+00	3.3437e-05	1.0236e-02	9.9053e-03	3.0322e+00
301.1225	1.5903e-02	9.9812e+00	8.7912e-06	1.1678e-03	5.6094e-03	7.4513e-01
965.8164	1.7428e-02	1.0044e+01	1.4605e-06	6.0490e-05	2.9022e-03	1.2020e-01

BJH desorption summary

Surface Area = 10.044 m²/g
Pore Volume = 0.017 cc/g
Pore Diameter Dv(d) = 35.886 Å





Analysis

Operator:nova
Sample ID: KTM-H2SO4
Sample Desc:
Sample weight: 0.1708 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 490.3 min
Cell ID: 92

Date:2018/09/20

Filename:
Comment:
Sample Volume: 0.0438 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:11:38

Report

Operator:nova Date:9/24/2018
C:\QCdata\Physisorb\KTM-H2SO4.qps

Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station C
FW version: 0.00

BJHPoreSizeDistribution Desorption

Data Reduction Parameters Data

t-Method	Calc. method: de Boer		
BJH/DHmethod	Moving pt. avg.: off	Ignoring P-tags below 0.35 P/Po	
Adsorbate	Nitrogen	Temperature	77.350K
	Molec. Wt.: 28.013 g	Cross Section:	16.200 Å ²
	Contact Angle: 0.0 degrees	Surf. Tension:	8.850 erg/cm ²
		Liquid Density:	0.808 g/cc

BJH Pore Size Distribution Desorption Data

Diameter	Pore Volume	Pore Surf Area	dV(d)	dS(d)	dV(logd)	dS(logd)
[Å]	[cc/g]	[m ² /g]	[cc/Å/g]	[m ² /Å/g]	[cc/g]	[cc/g]
35.8476	1.4223e-03	1.5870e+00	2.2736e-04	2.5369e-01	1.8719e-02	2.0887e+01
42.9504	2.5421e-03	2.6299e+00	1.4086e-04	1.3118e-01	1.3891e-02	1.2937e+01
52.6413	3.7218e-03	3.5264e+00	1.0320e-04	7.8415e-02	1.2459e-02	9.4673e+00
66.4088	4.6493e-03	4.0850e+00	5.7594e-05	3.4691e-02	8.7635e-03	5.2785e+00
88.1790	5.0086e-03	4.2480e+00	1.3096e-05	5.9406e-03	2.6374e-03	1.1964e+00
129.5572	5.7335e-03	4.4718e+00	1.3104e-05	4.0457e-03	3.8489e-03	1.1883e+00
264.2387	1.2115e-02	5.4378e+00	2.9815e-05	4.5133e-03	1.7101e-02	2.5887e+00
1206.4306	1.4345e-02	5.5118e+00	1.3348e-06	4.4255e-05	3.0117e-03	9.9854e-02

BJH desorption summary

Surface Area = 5.512 m²/g
Pore Volume = 0.014 cc/g
Pore Diameter Dv(d) = 35.848 Å





Analysis

Operator:nova
Sample ID: KTK
Sample Desc:
Sample weight: 0.1355 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 481.8 min
Cell ID: 62

Date:2018/09/20

Filename:
Comment:
Sample Volume: 0.03474 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:03:11

Report

Operator:nova
Date:9/24/2018
Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station A
F/W version: 0.00

Isotherm

Data Reduction Parameters Data

Adsorbate	Nitrogen	Temperature	77.350k
	Molec. Wt.: 28.013 g	Cross Section:	16.200 Å²
		Liquid Density:	0.808 g/cc

Isotherm Data

Relative Pressure	Volume @ STP [cc/g]	Relative Pressure	Volume @ STP [cc/g]	Relative Pressure	Volume @ STP [cc/g]
2.31600e-02	0.8967	4.93968e-01	4.3073	9.64071e-01	16.7477
5.93380e-02	0.9732	5.28409e-01	4.8591	9.89844e-01	19.3004
9.41970e-02	1.0056	5.57408e-01	5.3746	9.49875e-01	17.1600
1.23188e-01	1.0834	5.90771e-01	5.9481	8.68362e-01	15.4031
1.62312e-01	1.1927	6.24979e-01	6.6986	7.96456e-01	14.1268
1.90915e-01	1.3133	6.55691e-01	7.3024	7.19844e-01	12.7420
2.20362e-01	1.4492	6.84162e-01	8.0082	6.42456e-01	11.6668
2.50004e-01	1.6047	7.17611e-01	8.6867	5.62819e-01	10.6263
2.80716e-01	1.8565	7.50129e-01	9.3995	4.82648e-01	9.6236
3.11815e-01	2.1561	7.84469e-01	10.4791	4.06369e-01	8.6149
3.41906e-01	2.4226	8.05241e-01	11.2366	3.30617e-01	7.6647
3.72610e-01	2.7230	8.33169e-01	11.9988	2.53827e-01	6.5707
4.05012e-01	3.0404	8.69401e-01	12.8977	1.74973e-01	5.5145
4.35212e-01	3.4316	9.03889e-01	13.7983	9.51670e-02	4.3501
4.63396e-01	3.8418	9.32142e-01	15.0322		





Analysis

Operator:nova
Sample ID: KATK
Sample Desc:
Sample weight: 0.1046 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 485.6 min
Cell ID: 32

Date:2018/09/20

Filename:
Comment:
Sample Volume: 0.02682 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:06:55

Report

Operator:nova
Date:9/24/2018
Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station B
F/W version: 0.00

Isotherm

Data Reduction Parameters Data

Adsorbate	Nitrogen	Temperature	77.350k
	Molec. Wt.: 28.013 g	Cross Section:	16.200 Å ²
		Liquid Density:	0.808 g/cc

Isotherm Data

Relative Pressure	Volume @ STP [cc/g]	Relative Pressure	Volume @ STP [cc/g]	Relative Pressure	Volume @ STP [cc/g]
2.58730e-02	0.5487	4.99652e-01	3.5554	9.62032e-01	14.1222
5.97870e-02	0.6737	5.30720e-01	4.1166	9.86929e-01	16.1042
9.46240e-02	0.6874	5.60121e-01	4.4622	9.54682e-01	15.1827
1.23614e-01	0.7503	5.94299e-01	5.1758	8.67641e-01	13.7967
1.62917e-01	0.8536	6.25057e-01	5.6888	7.93153e-01	12.8911
1.89899e-01	0.9659	6.56086e-01	6.2754	7.15750e-01	11.9424
2.20959e-01	1.0808	6.87659e-01	6.8761	6.38455e-01	11.0537
2.51028e-01	1.2640	7.17874e-01	7.4267	5.64556e-01	10.1381
2.78149e-01	1.4807	7.49098e-01	8.1303	4.85207e-01	9.0853
3.11699e-01	1.6740	7.84702e-01	8.8721	4.06889e-01	8.1395
3.37836e-01	1.8759	8.08807e-01	9.4890	3.31920e-01	7.1310
3.74130e-01	2.1448	8.37480e-01	10.1752	2.54920e-01	6.0410
4.07369e-01	2.4049	8.75650e-01	11.0710	1.76609e-01	4.8494
4.35018e-01	2.7189	9.04044e-01	12.0257	9.52830e-02	3.5020
4.61256e-01	3.0413	9.30313e-01	12.8605		





Analysis

Operator:nova
Sample ID: KTM-H2SO4
Sample Desc:
Sample weight: 0.1708 g
Outgas Time: 3.0 hrs
Analysis gas: Nitrogen
Press. Tolerance: 0.050/0.050 (ads/des)
Analysis Time: 490.3 min
Cell ID: 92

Date:2018/09/20

Filename:
Comment:
Sample Volume: 0.0438 cc
OutgasTemp: 300.0 C
Bath Temp: 77.3 K
Equil time: 120/120 sec (ads/des)
End of run: 2018/09/20 1:11:38

Report

Operator:nova Date:9/24/2018
C:\QCdata\Physisorb\KTM-H2SO4.qps

Sample Density: 3.9 g/cc
Equil timeout: 240/240 sec (ads/des)
Instrument: Nova Station C
FW version: 0.00

Isotherm

Data Reduction Parameters Data

Adsorbate	Nitrogen	Temperature	77.350K	Liquid Density:	0.808 g/cc
	Molec. Wt.: 28.013 g	Cross Section:	16.200 Å ²		

Isotherm Data

Relative Pressure	Volume @ STP [cc/g]	Relative Pressure	Volume @ STP [cc/g]	Relative Pressure	Volume @ STP [cc/g]
2.37720e-02	4.8982	4.89750e-01	15.1386	9.55426e-01	31.5664
5.47550e-02	5.6503	5.25137e-01	15.9600	9.90519e-01	34.6540
8.84130e-02	6.2972	5.52973e-01	16.6760	9.45463e-01	33.2857
1.17846e-01	6.9472	5.87119e-01	17.6525	8.66431e-01	29.8626
1.57396e-01	7.6114	6.22483e-01	18.4139	7.91424e-01	29.4119
1.80882e-01	8.2150	6.50713e-01	19.2570	7.14726e-01	29.1629
2.14547e-01	8.8745	6.83790e-01	20.0672	6.39556e-01	28.7294
2.42886e-01	9.6349	7.15036e-01	20.8450	5.60160e-01	28.2239
2.72691e-01	10.2566	7.38855e-01	21.6178	4.84191e-01	27.7586
3.06977e-01	10.8929	7.76204e-01	22.5965	4.07106e-01	27.2105
3.37836e-01	11.5257	8.05225e-01	23.3894	3.31447e-01	26.5602
3.70090e-01	12.2110	8.33797e-01	24.2704	2.54726e-01	25.8245
4.02849e-01	12.8628	8.71223e-01	25.2664	1.76827e-01	24.9823
4.31366e-01	13.6529	8.96717e-01	26.9960	9.64380e-02	23.9069
4.60109e-01	14.3207	9.29498e-01	30.2055		

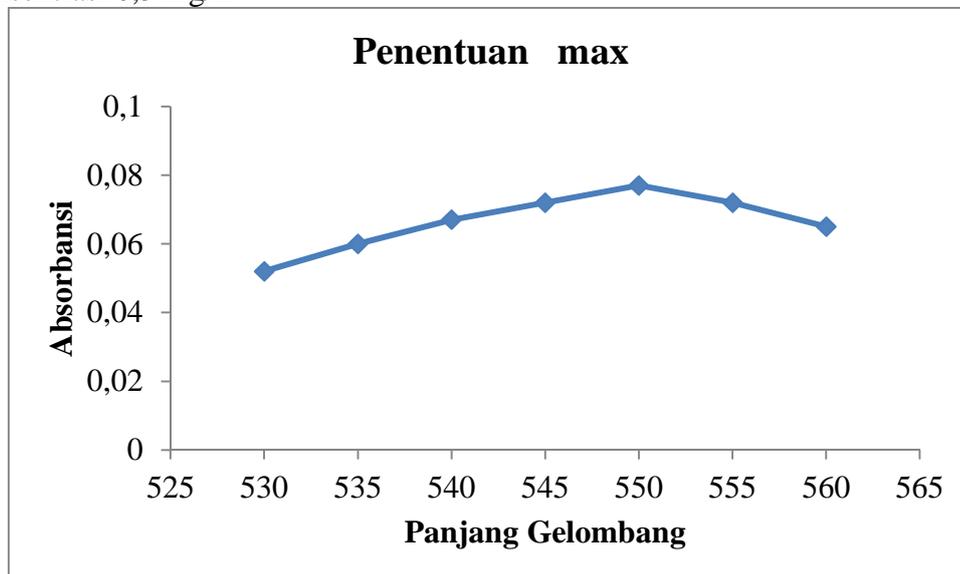


Lampiran 13. Data Penentuan Panjang Gelombang Maksimum Rhodamin B dengan Konsentrasi 0,3 mg/L.

Hubungan antar Absorbansi dan Panjang Gelombang rhodamin B dengan konsentrasi 0,3 mg/L

Panjang Gelombang	Absorbansi
530	0,052
535	0,06
540	0,067
545	0,072
550	0,077
555	0,072
560	0,065

Kurva hubungan antar Absorbansi dan Panjang Gelombang rhodamin B dengan konsentrasi 0,3 mg/L

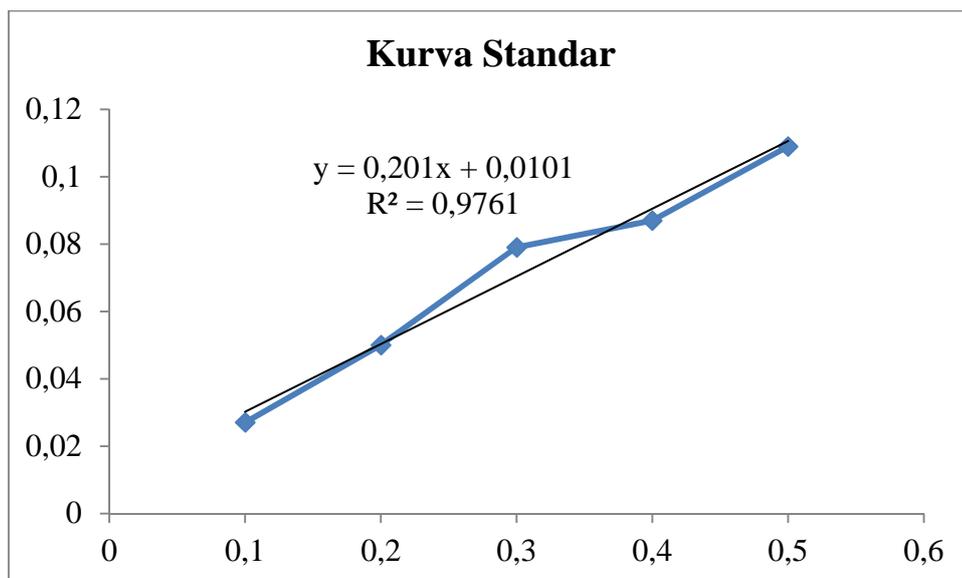


Lampiran 14. Data Absorbansi Kurva Standar Larutan Rhodamin B

Hubungan antar Absorbansi dan konsentrasi rhodamin B

Konsentrasi	Absorbansi
0,1	0,027
0,2	0,05
0,3	0,079
0,4	0,087
0,5	0,109

Kurva standar penentuan larutan rhodamin B dengan Spektrofotometer Uv-Vis



Lampiran 15. Penentuan Waktu Optimum Adsorpsi Rhodamin B oleh Karbon Aktif Tempurung kluwak Termodifikasi H₂SO₄

Data Penentuan Waktu Optimum Adsorpsi Rhodamin B Karbon Aktif Termodifikasi

Waktu Kontak	Absorbansi	C_e (mg/L)	C_o (mg/L)	W_a (g)	q_e (mg/g)
1 menit	0,342	1,651243781	30	0,5006	2,438417183
3 menit	0,114	0,516915423	30	0,5004	2,552733932
5 menit	0,027	0,084079602	30	0,5001	2,597540193
10 menit	0,011	0,004477612	30	0,5002	2,604977909
15 menit	0,011	0,004477612	30	0,5005	2,603416484
20 menit	0,012	0,009452736	30	0,5006	2,602399509
25 menit	0,011	0,004477612	30	0,5007	2,602376573
30 menit	0,015	0,024378109	30	0,5006	2,60090876

Contoh perhitungan jumlah rhodamin B yang diadsorpsi (q_e) pada t = 10 menit (persamaan 7)

$$q_e = \frac{(30 - 0,004477612) \frac{\text{mg}}{\text{L}}}{0,5002 \text{ g}} \times 0,05 \text{ L}$$

$$= 2,604977909 \text{ mg/g}$$



Lampiran 16. Data Kinetika Reaksi Orde Satu Semu dan Orde Dua Semu Rhodamin B oleh Karbon Aktif Tempurung Kluwak Termodifikasi

Waktu (menit)	q_t (mg/g)	q_e (mg/g)	$(q_e - q_t)$	$\log(q_e - q_t)$	t/q_t
1	2,438417183	2,604977909	0,166560726	-0,778427395	0,410102097
3	2,552733932	2,604977909	0,052243977	-1,28196377	1,175210609
5	2,597540193	2,604977909	0,007437716	-2,128560409	1,92489803
15	2,603416484	2,604977909	0,001561425	-2,806478871	5,761659762
20	2,602399509	2,604977909	0,0025784	-2,588649707	7,685215099
25	2,602376573	2,604977909	0,002601336	-2,584803549	9,606603541
30	2,60090876	2,604977909	0,004069149	-2,390496407	11,53442999

Data grafik kinetika orde satu semu diperoleh persamaan garis:

$$y = -0,0504x - 1,367$$

dari persamaan garis diperoleh nilai *slope* (a) = -0,0504 dan *intercept* (b) = -1,367

Nilai k_1 dapat dihitung sebagai berikut:

$$Slope = -\frac{k_1}{2,303}$$

$$k_1 = -(slope \times 2,303)$$

$$= -(-0,0504 \times 2,303)$$

$$= 0,1161 \text{ menit}^{-1}$$

Nilai adsorpsi dapat dihitung sebagai berikut:

$$Intercept = \log q_e$$

$$q_e = \text{invers log}(-1,367)$$

$$= 0,0429 \text{ mg/g}$$

Grafik kinetika orde dua semu diperoleh persamaan garis:

$$y = 0,3836x + 0,0174$$



dari persamaan garis diperoleh nilai *slope* (a) = 0,3836 dan *intercept* (b) = 0,0174

$$\text{Slope} = \frac{1}{q_e}$$

$$q_e = \frac{1}{0,3836}$$

$$q_e = 2,6069 \text{ mg/g}$$

$$\text{Intercept} = \frac{1}{k_2 q_e^2}$$

$$k_2 = \frac{1}{(0,0174) \times (2,6069)^2}$$

$$k_2 = 8,4602 \text{ g.mg}^{-1}.\text{menit}^{-1}$$



Lampiran 17. Penentuan Kapasitas Adsorpsi Rhodamin B oleh Karbon Aktif Termodifikasi

C_o (mg/L)	Absorbansi	C_e (mg/L)	x/m atau q_e (mg/g)	C_e/q_e	log C_e	log q_e
25,8656	0,007	0,0990	2,5756	0,0384	-1,0043	2,5756
50,7412	0,935	5,0492	4,5682	1,1052	0,7032	4,5682
78,8308	0,59	28,8507	4,9970	5,7736	1,4601	4,9970
121,368	1,19	58,7014	6,2641	9,3710	1,7686	6,2641
160,6716	0,39	94,5024	6,6129	14,2905	1,9754	6,6129
193,0099	0,508	123,8557	6,9126	17,9172	2,0929	6,9126
257,4378	0,8	196,4925	6,0884	32,2730	2,2933	6,0884

Contoh perhitungan jumlah rhodamin B yang diadsorpsi (q_e) pada konsentrasi 257,4378109 (persamaan 7)

$$q_e = \frac{(257,4378-196,4925) \frac{\text{mg}}{\text{L}}}{0,5005 \text{ g}} \times 0,05 \text{ L}$$

$$= 6,0884 \text{ mg/g}$$



Lampiran 18. Contoh Perhitungan nilai Q_0 dan b

Berdasarkan model isotermal Langmuir diperoleh persamaan garis :

$$. y = 0,1572x + 0,1385$$

dari persamaan garis tersebut, nilai *slope* = 0,1572 dan *intercept* 0,1385

(persamaan 9)

$$\frac{1}{Q_0} = \text{kemiringan (slope)}$$

$$\frac{1}{Q_0} = \text{tg}$$

$$Q = \frac{1}{\text{slope}}$$

$$= \frac{1}{0,1572}$$

$$= 6,3613 \text{ mg/g}$$

$$\frac{1}{Q_0 b} = \text{intercept}$$

$$b = \frac{1}{Q_0 \times \text{intercept}}$$

$$= \frac{1}{6,3613 \frac{\text{mg}}{\text{g}} \times 0,1385 \text{ g/L}}$$

$$= 1,1350 \text{ L/mg}$$

Berdasarkan model isotermal Freundlich diperoleh persamaan garis :

$$1,3502x + 3,7475$$

dari persamaan garis tersebut, nilai *slope* = 1,3502 dan *intercept* = 3,7475

(persamaan 8)

intercept

invers log intercept



$$= \text{invers log } -3,7475$$

$$= 0,0002 \text{ mg/g}$$

$$\frac{1}{n} = \text{kemiringan (slope)}$$

$$n = \frac{1}{\text{slope}}$$

$$= \frac{1}{1,3502 \frac{\text{L}}{\text{g}}}$$

$$= 0,7406 \text{ g/L}$$



Lampiran 19. Desorpsi

Pendesorpsi	Kons. Sebelum Desorpsi	Setelah Desorpsi		Rasio Desorpsi (%)
		Abs	Kons.	
HCl	12,7840796	0,013	0,014427861	11,29%
HNO ₃		0,011	0,004477612	3,50%
H ₂ O		0,015	0,024378109	19,07%

$$\text{Rasio desorpsi} = \frac{\text{jumlah zat warna yang didesorpsi}}{\text{jumlah zat warna yang teradsorpsi}} \times 100\%$$

$$\begin{aligned} \text{Rasio desorpsi} &= \frac{0,024378109}{12,7840796} \times 100\% \\ &= 0,1906912 \% \end{aligned}$$

