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Lampiran 1 *Master* Tabel Penelitian

Parameter	Hari		
	1	2	3
Data PT. Eastern Pearl Flour Mills			
Parameter Boiler			
Tekanan produk uap ($kg/cm^2/h$)	7,32	7.54	7.20
Laju Konsumsi Bahan Bakar (kg/h)	88,57	100,42	96,04
GCV Biosolar (kkal/h)	10.702	10.702	10.702
Karbon (C) (wt%)	81,8	81,8	81,8
Oksigen bahan bakar (O_2) (wt%)	5,68	5,68	5,68
Nitrogen (N) (wt%)	0	0	0
Sulfur (S) (wt%)	0,073	0,073	0,073
Hidrogen (H_2) (wt%)	12,4	12,4	12,4
Oksigen gas buang (O_2) (%)	11,6	11,6	11,6
Karbondioksida (CO_2) (%)	6,16	6,16	6,16
Nitrogendioksida (NO_2) (%)	0,5	0,5	0,5
Tempratur gas buang (Tf) (°C)	231,2	229,8	233,4
Temperatur ruangan (Ta) (°C)	31,3	30.6	31.7
Kalor spesifik gas buang (cpf) ($kkal/kg^oC$)	1,02	1,02	1,02
Kalor spesifik uap (cps) ($kkal/kg^oC$)	0,25	0,25	0,25
Kelembaban (kg/kg dry air)	0,021	0,021	0.021
Laju Massa Uap (kg/h)	934,35	956,77	921,82
TDS air umpan (S) (PPM)	61	61	61
TDS air boiler (C_a) (PPM)	415	415	415
Max. TDS rekomendasi (C) (PPM)	3000	3000	3000
Parameter Pipa Boiler ke Boiler Header			
Massa jenis fluida (ρ) (kg/m^3)	3,748	3,856	3,695
Kecepatan fluida dalam pipa (V) (m/s)	3,769	3,763	3,711
Viskositas dinamika fluida (μ) (N/m^2)	$14,57\times10^{-6}$	$14,61\times10^{-6}$	$14,55\times10^{-6}$
Parameter Pipa Boiler Header ke Pelletizing Header			
Massa jenis fluida (ρ) (kg/m^3)	3,392	3,178	3,402
Kecepatan fluida dalam pipa (V) (m/s)	2,392	2,343	2,393
Viskositas dinamika fluida (μ) (N/m^2)	$14,42\times10^{-6}$	$14,33\times10^{-6}$	$14,43\times10^{-6}$

Lampiran 2 Dokumentasi Penelitian